

FILE: 5340-20



DATE: July 5, 2017

Chair and Members

Comox Valley Sewage Commission

FROM: Russell Dyson

Chief Administrative Officer

RE: Comox Valley Water Pollution Control Center – Alternate Option for Phase 1 Upgrades

Purpose

TO:

To provide an alternate option to the already approved phase one upgrades at the Comox Valley Water Pollution Control Center (CVWPCC).

Policy Analysis

The Comox Valley Regional District (CVRD) operates a sewerage service primarily for the City of Courtenay and Town of Comox, established by Bylaw No. 2541, being the "Comox Valley Sewerage Service Establishment Bylaw No. 2541, 2003".

At their November 15, 2016 meeting the Comox Valley Sewage Commission passed the following motion:

THAT the Comox Valley Regional District proceed with planning, engineering and construction of phase one of the Comox Valley Water Pollution Control Center (CVWPCC) upgrade option three identified within the CVWPCC Capacity Assessment completed by ISL Engineering and Land Services dated August 2016;

AND FINALLY THAT as part of the phase one upgrades for the CVWPCC, ultraviolet disinfection technology with a disinfection target of 200MPN/100mL be included within the scope of work for the detailed design.

Executive Summary

To better understand the capital upgrades and operational requirements required to service a growing population and changing regulations, a capacity assessment of the treatment plant and outfall was conducted in 2016 by ISL Engineering and Land Services (ISL) along with an ultraviolet (UV) disinfection feasibility study completed by AECOM.

Through ISL's work a recommended option was developed that improved plant capacity along with improving effluent quality to comply with *Municipal Wastewater Regulations* (MWR). The recommended option included installation and replacement of the mechanical screen and grit removal system, construction of an offline equalization tank, a reclaimed water service and installation of UV disinfection equipment and a cloth media filter.

In November 2016, the Sewage Commission approved proceeding with planning, engineering and construction of the phase one upgrades as identified by ISL within their capacity assessment. Due to the significant capital costs of the recommended upgrades and the multi-year approach, the CVRD undertook an independent third party review of ISL's findings prior to proceeding with the detailed

design. The purpose of the third party review was to review ISL's recommendation and identify efficiencies.

From this third party review an alternate option was suggested that replaces addition of a cloth media filter at this time with construction of a fourth clarifier. This option was reviewed in detail by ISL (memorandum attached as Appendix A) and was determined to significantly reduce the initial capital cost, while providing effluent quality that will still meet the anticipated MWR effluent quality requirements.

Table No.1 below compares capital and operating costs along with providing a net present value analysis for the original option (option three) and the proposed new option (option nine)

Table No.1: Comparison of Costs

Description	Original Option (Option Three)	Proposed New Option (Option Nine)
Phase 1 - 2017 Construction	\$15,489,000	\$12,327,000
Phase 2 - 2024 Construction	\$6,610,000	\$6,610,000
Phase 3 – Construction years vary	\$46,983,000	\$44,520,000
Total Capital Costs	\$69,082,000	\$63,457,000
Estimated Yearly Operating Costs	\$68,000	\$50,000
Net Present Value	\$53,637,000	\$48,312,000

Both option three and option nine include the addition of an offline equalization process to reduce peak hourly flows during peak wet weather events. Option nine provides reduced capital costs and will meet all current regulations but will not provide tertiary treatment. Should total suspended solids (TSS) regulations be tightened in the future a cloth media filter could be added then.

Recommendation from the Chief Administrative Officer:

THAT the Comox Valley Regional District proceed with planning, engineering and construction of the phase one upgrades at the Comox Valley Water Pollution Control Center as per the alternate option (option nine) as identified within the Wastewater Treatment Option Memorandum completed by ISL Engineering and Land Services dated June 27, 2017.

Respectfully:	
R. Dyson	
Russell Dyson	
Chief Administrative Officer	

Background/Current Situation

The 2011 CVRD sanitary sewerage master plan and long term financial plan both identify the need for capital upgrades to the CVWPCC. The original facility was commissioned in 1984 and has undergone expansions in 1993 and 2008. As population and flows increase, upgrades are required for capacity increases to accommodate growth. Upgrades to alleviate capacity concerns will trigger the requirement for the CVWPCC to become registered under the MWR. These more stringent regulations require additional upgrades to improve effluent quality in order to be in compliance with the MWR.

To better understand the capital upgrades and operational requirements required to service a growing population and more stringent regulations, a capacity assessment of the treatment plant and outfall was conducted along with an UV disinfection feasibility study in 2016. The CVWPCC

capacity assessment, completed by ISL, provided a recommended phased upgrade approach that increases capacity and improves effluent quality. The UV feasibility study recommended UV disinfection targets and provided sizing and costing information.

The first phase of the recommended upgrades are required to alleviate current plant capacity constraints, as well as ensuring MWR redundancy and effluent quality requirements are achieved. MWR guidelines for effluent quality include TSS below 25mg/L and a disinfection step to ensure fecal coliform counts are below the limits at the edge of the initial dilution zone. The original preferred option by ISL included the addition of an equalization tank after the primary clarifiers to reduce peak hour flows, a cloth media filter, and installation of UV disinfection equipment. The installation of the cloth media filter would provide tertiary treatment for the plant and would optimize UV disinfection equipment, provide an opportunity for greater water reuse throughout the plant and provide a physical barrier to ensure the TSS consistently remains below 10mg/L.

Due to the significant capital costs of the recommended upgrades and the multi-year approach, the CVRD decided to complete an independent third party review of ISL's findings prior to proceeding with the detailed design. The purpose of the third party review being primarily to review ISL's recommendations and identify any alternative options that may provide cost efficiencies.

Through this process an alternate option was identified that includes an equalization tank but instead of a cloth media filter the option includes the construction of a fourth clarifier to improve performance during periods of higher flows.

The CVWPCC currently operates in three distinct trains, each train is comprised of a primary clarifier, bioreactor and secondary clarifier. The typical depth of secondary clarifiers is four to five meters deep, however the two original clarifiers are shallow with a depth of 3.1meters. Deeper clarifiers help to ensure the sludge blanket is further away from the effluent weir and therefore solids escapement through the effluent is less likely. Both ISL and the third party reviewer identified the shallow clarifiers as a problem, but whereas ISL proposed a fabric filter to compensate, the third party reviewer has recommended an additional clarifier.

The proposed new option requires all the same upgrades as previously approved, but replaces the installation of the cloth media filter with a fourth clarifier. The new option will not provide tertiary treatment but will provide effluent that meets the anticipated MWR requirements of 25 mg/L of TSS. Should TSS requirements be tightened in the future the CVWPCC will still have the ability to add a cloth media filter at such time.

CVRD management and operators have maximized use of effluent for plant processes but the CVWPCC remains a large potable water consumer. The quality of water to be produced by the fabric filter would have allowed the plant to eliminate potable water use for plant processes, saving approximately \$35,000 per year. Option nine evaluated by ISL includes installation of an effluent reuse filtration package that would provide the CVWPCC with enough treated water to displace use of potable water for plant processes.

Table No. 2 below highlights the costs of the two alternate phase one upgrade options at the CVWPCC.

Table No. 2: Capital Cost Comparison of Options for CVWPCC Phase One Upgrades

Project Description	Requirement	Original Option (Option Three)	Proposed New Option (Option Nine)
Repair existing offshore pipe	Capacity/ Environmental	\$168,000	\$168,000
Mechanical screen/grit removal	Capacity	\$2,067,800	\$2,067,800
Construct offline equalization tank	Capacity	\$5,847,800	\$5,847,800
Install UV disinfection(MWR compliance)	Effluent Quality	\$3,115,000	\$3,115,000
Add cloth media filter	Effluent Quality	\$7,404,600	-
Construct fourth clarifier	Effluent Quality	-	\$3,035,200
Reclaimed water service	Capacity	\$375,000	\$375,000
Effluent reuse filtration package (optional)	Capacity/Reuse Quality		\$1,208,200
Total Phase 1 Capital Costs		\$18,979,000	\$15,817,000

As can be seen in Table No. 2, the capital costs for option nine are significantly less than the original proposed option three. Further upgrade phases will remain the same with the exception of reduced costs in phase three as no cloth media filter upgrades would be required. The original option three identified the potential for cost savings for the UV equipment with the installation of a cloth media filter, but these are likely to be modest operational cost savings rather than a reduction in capital costs.

A net present value analysis for the two options over a 50 year period was completed. Table No. 3 below details the capital, operating and NPV analysis for each option over a 50 year time period. The NPV analysis does not include operational costs for UV.

Table No. 3: Comparison of Costs

Description	Original Option (Option Three)	Proposed New Option (Option Nine)
Total capital costs (all phases)	\$69,082,000	\$63,457,000
Estimated yearly operating costs	\$68,000	\$50,000
Net Present Value	\$53,637,000	\$48,312,000

As identified by ISL both option three and option nine are viable and can be incorporated into the existing treatment plant. Option nine provides some distinct cost saving advantages, with both decreased capital and estimated yearly operating costs. Option nine will meet current MWR requirements for effluent quality however will not provide tertiary treatment and subsequently a physical barrier for the effluent to ensure that TSS will never exceed permit limits during peak flow events. Should TSS regulations become stricter in the future, a cloth media filter could still be added at a later date to comply with these changes.

Options

The Comox Valley Sewage Commission has the following options to consider:

1. Proceed with the alternate upgrade option as outlined in ISL's Wastewater Treatment Options Memorandum dated June 27, 2017.

- 2. Proceed with the previously approved upgrades to the CVWPCC as per option three as outlined within ISL's CVWPCC capacity assessment report dated August 2016.
- 3. To not proceed with upgrades at this time.

Proceeding with option 1 will allow the CVWPCC to comply with the anticipated MWR effluent quality requirements at a significantly lower capital cost than that of the installation of a fabric filter. As such only option 1 above is recommended.

Financial Factors

An updated 10 year capital plan was approved by the Comox Valley Sewage Commission in November 2016 and included \$18,638,200 for the phase one capacity and effluent quality upgrades at the CVWPCC. Modifying the scope of the phase 1 upgrades will reduce the capital costs and associated borrowing requirements for this project.

Legal Factors

Upgrades to the CVWPCC will require registration under the MWR. The recommended improvements to the CVWPCC will ensure that the plant is compliant under the more stringent MWR requirements.

Regional Growth Strategy Implications

Upgrades to the CVWPCC will help ensure proper and effective treatment of wastewater for future generations whilst supporting a high quality of life through the protection and enhancement of community health and safety.

Disinfection of the effluent will add improved redundancy within the treatment process, compliance with regulations and increase local shellfish harvesting security by ensuring fecal coliform limits at the end of pipe are below guidelines.

Intergovernmental Factors

The Comox Valley Sewerage Service is governed by the Sewage Commission whose membership includes representation from the Town of Comox, the City of Courtenay and the Department of National Defence.

Interdepartmental Involvement

The Engineering Services Branch is leading this work.

Citizen/Public Relations

The CVWPCC is requiring significant upgrades in order to increase capacity and accommodate growth. The CVRD Engineering Services will be working closely with the communications department to keep the public up to date on the facility expansion.

Prepared by:	Concurrence:	Concurrence:
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Attachments: Appendix A - "Wastewater Treatment Options Memorandum, completed by ISL

Engineering and Land Service dated June 27, 2017"

Appendix A





Inspiring sustainable thinking



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To: Comox Valley Regional District Date: June 27, 2017

Attention: Charlie Gore, Manager Capital Projects Project No.: 31548

Cc: Kris La Rose, P.Eng.

Reference: Wastewater Treatment Options

From: **Ashraf Rayyan, P.Eng., PMP.**

1.0 Introduction

1.1 Authorization

ISL Engineering and Land Services (ISL) was retained by the Comox Valley Regional District, "The District" to investigate the possibility of adding a fourth secondary clarifier to the Comox Valley Water Pollution Control Centre (CVWPCC). The scope of work was authorized by the District in response to ISL's proposal dated June 16, 2017.

1.2 Background

In August 2016, ISL completed "CVWPCC Capacity Assessment Study", which assessed existing treatment units. The study provided a clear path for upgrading the existing treatment process units up to 2066. The study developed several treatment options (8 options) and shortlisted (3 options) for further evaluation. The shortlisted options were evaluated in a more detail and ISL recommended Option 3 for implementation.

Option 3 requires the addition of an equalization process downstream of the primary clarifiers to reduce peak hourly flows during peak wet weather events, which will minimize the escaping of solids into the effluent. Incorporating the equalization tank will minimize the hydraulic shock load to the biological treatment. This option also includes the addition of cloth media disk filters as tertiary treatment (after the secondary clarifiers) to minimize the escaping of solids into the effluent during peak wet weather events. This option will not eliminate the need of a new bioreactor tank and clarifier, however, it will delay their construction to 2024. Process flow diagram and proposed conceptual plant layout for option 3 is included in Appendix B.

Option 3 may require adding polymer prior to the cloth media filter to enhance the filtration step. This option will provide a better effluent quality (TSS less than 10 mg/L) and a particle size less than 30 microns for optimum UV performance.

1.3 Scope of Work

Following additional discussion, the District directed ISL to investigate adding a fourth secondary clarifier to enhance the clarification process (Option 9), in lieu of constructing a cloth media filter for effluent polishing (Option 3). This memorandum addresses the viability, advantages and disadvantages of the option.



1.4 Existing Condition

The plant has three distinctive trains. Each train is comprised of a primary clarifier, bioreactor and secondary clarifier. Each bioreactor feeds its own secondary clarifier, and each train is provided with its return sludge pump. The ISL assessment report (2016) evaluated the existing biological treatment and found that the capacity of the existing bioreactors and secondary clarifiers are sufficient up to year 2019 and 2033 respectively.

Because the bioreactors and secondary clarifiers are normally constructed in tandem, ISL recommended that an additional bioreactor and secondary clarifier to be constructed by 2024 for Option 3 Phase 2 with full understanding that the plant may operate (from 2017 to 2023) on a higher mixed liquor suspended solids (MLSS) rate of 2500 mg/L which is higher than the target goal of 2300 mg/L and cloth media filter can provide an added protection for reducing TSS in the effluent. The plant can achieve MLSS 2500 mg/L when the Sludge Volume Index (SVI) is less than (150 mL/g). However, when the SVI is more than 250 mL/g, the plant reduces its MLSS to 2000 mg/l or less to minimize upsetting of the existing clarifiers. The existing bioreactors (2019) and secondary clarifiers (2033) are assessed based on a MLSS of 2000 mg/L.

In assessing the secondary clarifiers, the following were indicated in the ISL study:

- Based on the current flows, the plant can achieve an average monthly TSS of 25 mg/L (most of the time). It is
 anticipated that the influent flow will increased in the future, and the treatment capacity will need to be increased
 to handle future flows.
- Secondary clarifiers are typically designed based on overflow rates and solids loading rates, with the former being considered more important for operation and design purposes. Typical values for overflow rates and solids loading rates are available from different sources, these typical values are based on a clarifier depth of 4.0 to 5.5 m. The existing treatment facility has three clarifiers, two with a depth of 3.13 m each and one with a depth of 5.0 m. The clarifiers constructed in 1982 have a depth less than the typical depth of a secondary clarifier (4.0 5.5 m) as well as the depth of the clarifier constructed in 2008. A tank with a greater depth would be able to keep the sludge blanket further away from the effluent weir and better performance is normally achieved with such tanks.
- The plant has poor sludge settleability condition. Sludge settleability reflects the biological health of microorganisms within the bioreactor tanks but is only noticeable in the clarifier. Poor settling sludge causes the sludge blanket to rise to the surface, thus resulting in loss of solids in the effluent. The Sludge Volume Index (SVI) is commonly used for measuring sludge settleability. A review of the 2015 facility operating data indicates that the average operating SVI is 261 mL/g, which is high compared to a typical value of 150 mL/g or less.
- The SVI can be improved by adding polymers, without causing a significant increase in the waste sludge production. Polymers are usually added to the MLSS as it leaves the bioreactor basin or to the secondary clarifier center well. A polymer supply company should be consulted for selection of the polymer and its dosage. Jar testing should be performed to determine the type of polymer needed and its dosage. The facility should target an SVI of 100 mL/g or less.

2.0 **Option 9**

Option 9 requires addition of an equalization process after the primary clarifiers to reduce peak hourly flows during peak wet weather events, which will minimize escaping of solids into the effluent. This option also includes addition of a fourth secondary clarifier to minimize escaping of solids into the effluent. Process flow diagram and proposed conceptual plant layout for option 9 is included in Appendix B



In this option, the flow from one of the bioreactors (1 or 2) will be directed to the two shallow clarifiers (3.13 m depth). The new clarifier will serve either one of the existing bioreactors (1 or 2). This option will not eliminate the need of new bioreactor and clarifier (2024), however, it will delay their construction to 2024. This option will provide TSS less than 25 mg/L. This option includes a filtration package unit for effluent reuse.

2.1 Clarifier, splitter and piping

The new clarifier will be similar to the existing clarifier # 3 (5.0 m water depth). Table 1.1 summarizes the new clarifier dimensions.

Table 1.1 - Fourth Clarifier Dimensions

Description	Units	Values
Number of secondary clarifiers		1
Shape		
Diameter	m	23.1
Water Depth	m	5.00
Area	m²	419

For this option, a small splitter box will be required to split the flow to the shallow clarifiers. Pipes modifications are required for the RAS/WAS pipes to accommodate the fourth clarifier, these modifications include yard piping and pipes within the congested pumps gallery.

2.2 Effluent Reuse

The MWR includes four categories of reclaimed water. Each category has specific quality and monitoring requirements, as prescribed in the respective tables and sections of MWR.

Indirect Potable Reuse: this category includes replenishment of a potable water source or potential potable water source, and any other application, including food crops and urban reuse, where a very high level of quality is warranted.

Greater Exposure Potential: this category includes agricultural crops, golf courses, cemeteries, residential lawns, greenhouses, silviculture operations, urban reuse and landscaping around parks, playgrounds, schools. Irrigation for frost protection and crop cooling is also permitted.

Moderate Exposure Potential: this category include may be selected when public contact is unlikely, the users are well aware of the risks posed by the use, and there will be no detrimental impact to the receiving environment from the use.

Lower Exposure Potential: this category is typically used in commercial or industrial applications where public access is restricted and where there will be no detrimental impact to the receiving environment from the use.



Table 2.1 summarizes the reclaimed water quality requirement for each category.

Table 2.1 – Muncipal Effluent Quality Requirements (Table 13 – MWR)

Parameters	Indirect Potable Reuse	Greater Exposure Potential	Moderate Exposure Potential	Lower Exposure Potential
pН	site specific	6.5 to 9	6.5 to 9	6.5 to 9
BOD5, TSS	BOD5 5 mg/L TSS < 5 mg/L	10 mg/L	25 mg/L	45 mg/L
turbidity	maximum 1 NTU	average 2 NTU, maximum 5 NTU	n/a	n/a
fecal coliform (/100 mL)	median < 1 CFU or < 2.2 MPN	median < 1 CFU or < 2.2 MPN; maximum 14 CFU	median 100 CFU; maximum 400 CFU	median 200 CFU; maximum 1 000 CFU

The plant staff intend to use the reclaimed water for plant irrigation, equipment and tanks washing. The Operators will be exposed to the reclaimed water. Both categories (greater exposure potential and moderate exposure potential can be applied for the treatment plant). If category "Moderate Exposure" is chosen, no treatment required other than chlorine disinfection. Adequate chlorine must be maintained and present at the point of use (minimum 0.5 mg/L).

If the category of "Greater Exposure Potential" is chosen, a filtration system complete with chlorine disinfection will be required. Using a modular unit of cloth media filter can achieve the required filtration step. The equipment is compact and can be installed indoor or outdoor of the UV building. Adequate chlorine must be maintained and present at the point of use (minimum 0.5 mg/L). For cost estimating purposes, ISL included the cost of the effluent filtration package. The package cost is based on the following;

- Installing the system indoor within the UV building
- Modular cloth filter system with a capacity of 1 MLD



2.3 Phasing

Table 2.2 provides the phasing for Option 9

Table 2.2: Options 9 Upgrades and Proposed Implementation Schedule

Phases	Construction	Population	Average Flow	Option 9	
	Year	Capita	MLD	Sphon 3	
Phase I (2017)	2017	Current		 Replace existing 12 mm mechanical screen with 6 mm screen Add grit removal tank c/w cyclones and classifiers units Decommissioning of existing primary sludge cyclones and classifiers and send the primary sludge directly to the sludge thickeners Injecting polymers prior existing clarifiers (provision to be confirmed by pilot testing) Add fourth clarifier Construct offline equalization tank Repair of existing offshore pipe Incorporate a UV disinfection Add effluent reuse filtration package (Optional) 	
Phase II (2024)	2024	50,109	21.1	Construct one aeration tank and clarifier	
	2031	55,017	23.2	Replace all outfall sections (onshore/offshore)	
	2033	57,189	23.8	Construct two primary clarifiers Construct new process building	
·	2,034	57,266	20.0	Expand Equalization Tank	
	2,043	64,576	22.6	Upgrade effluent pumps	
Phase III (Varies)	2045	66,786	28.0	Add mechanical screens to new process building Add grit removal tank c/w cyclones and classifiers units	
	2056	76,169	0.0	Construct new thickener	
	2060	81,280	0.0	Install new centrifuge	
	2063	85,140	0.0	Construct one aeration tank and clarifier	
Phase IV (Ultimate)	Beyond 2066 Beyond 2066			Construct One primary clarifier Construct one aeration tank and clarifier	



3.0 Financial Analysis

In order to fully evaluate Option 9 both capital and operational cost estimates were produced and have been summarized in Table 3.1, 3.2 and 3.3. The cost estimate shows also Option 3, recommended by ISL 2016 for comparison purposes.

A further detailed breakdown is provided in Appendix A of this report.

3.1 Capital Costs

The estimated capital costs within Table 3.1, 3.2 and 3.3 are considered to be at a conceptual level (Class D). A contingency of 40% is included in the cost estimates for engineering and construction contingencies. Furthermore no costs have been included within these estimates for the following:

- Land Procurement
- Taxes
- UV disinfection (included in AECOM report, 2016)
- Chlorine disinfection (included in AECOM report 2016)
- Non potable water pumping system (included in AECOM report, 2016)

All costs are represented in 2016 -Dollars

Table 3.1: Estimated Capital Cost Summary (2017)

Phase 1 - 2017 Construction					
Description	Option 3	Option 9			
Mechanical Screen	\$452,000	\$452,000			
Grit Removal	\$1,025,000	\$1,025,000			
Offline Equalization Tank	\$4,177,000	\$4,177,000			
Repair of existing outfall pipe	\$120,000	\$120,000			
Media Cloth Filter	\$5,289,000				
Fourth clarifier		\$2,168,000			
Effluent reuse filtration package (Optional)		\$863,000			
Capital Costs	\$11,063,000	\$8,805,000			
Engineering and Contingencies (40%)	\$4,426,000	\$3,522,000			
Total Capital Costs	\$15,489,000	\$12,327,000			

Table 3.2: Estimated Capital Cost Summary (2024)

Phase 2 - 2024 Construction					
Description Option 3 Option 9					
Biological Treatment	\$4,721,000	\$4,721,000			
Capital Costs	\$4,721,000	\$4,721,000			
Engineering and Contingencies (40%)	\$1,889,000	\$1,889,000			
Total Capital Costs	\$6,610,000	\$6,610,000			

Table 3.3: Estimated Capital Cost Summary (2031 – 2063)



Phase 3 - Construction Years (Varies)				
Description	Option 3	Option 9		
Replace Outfall Sections (Onshore/Offshore) - Year (2031)	\$13,949,000	\$13,949,000		
Primary Clarifiers + Process Building - Year (2033)	\$7,651,000	\$7,651,000		
Upgrade Media Cloth Filter - Year (2034)	\$1,759,000			
Effluent Pumps - Year (2043)	\$1,780,000	\$1,780,000		
Mechanical Screen - Year (2045)	\$892,000	\$892,000		
Grit Removal - Year (2045)	\$1,013,000	\$1,013,000		
Expand Chemical Treatment - Year (2045)	\$-	\$-		
Thickener - Year (2056)	\$1,072,000	\$1,072,000		
Centrifuge - Year (2060)	\$1,190,000	\$1,190,000		
Aeration Tank and Clarifier - Year (2063)	\$4,253,000	\$4,253,000		
Capital Costs	\$33,559,000	\$31,800,000		
Engineering and Contingencies (40%)	\$13,424,000	\$12,720,000		
Total Capital Costs	\$46,983,000	\$44,520,000		

3.2 Operating Costs

Detailed breakdown is included in Appendix A. The assumptions used for calculating the operating costs are as follows:

- Option 3 and 9: Operation of the equalization tank and equalization mixing will be intermittent, approximately 500 hrs. /year.
- Operation of Effluent Pumps will be intermittent, approximately 80 hrs. /year.
- For all options, operating costs for all equipment are not included in the operating costs, and we considered them equal for all options, with the exception of the following:
 - mixing and pumping power costs for the offline equalization tanks (Option 3 and 9)
 - cloth media disk filter and backwash pumps power costs and filter media replacement cost (Option 3)
 - Fourth clarifier power cost and repair/replacement costs (Option 9)
 - Effluent filtration package, power cost and repair/replacement costs (Option 9)
 - Effluent pumping (Option 3 and 9)
 - Heating and ventilation for UV/disk filter building (Option 3 and 9)
- Average yearly operating costs do not include the new UV system

For Options 3, the estimated extra solids production as a result of incorporating the cloth media filter into the process is 5.6 – 11.2 metric tons/year for years 2017 and 2062 respectively. ISL assumed that the cost of solids processed at the composting facility is equal to the selling revenue. Therefore, operating costs do not include any processing cost for the solids captured by the cloth media filter.



Average power are estimated based on the following.

- Pump and motor efficiencies 75%
- Mixing and Cloth media motors efficiency 90 %
- Clarifier motor efficiency 90%
- Effluent filtration package 75%
- Electrical power cost 0.1\$/kWh

For Options 3 and 9, upgrading of the existing effluent pumps by 2043 is required, the equalization tank will help to mitigate hourly variations in flowrates to obtain a nearly constant flowrate over the day. It is anticipated by 2043, the combined capacity of the equalization tank and the existing effluent pumps will be no more sufficient to normalize the maximum hourly flow to the maximum daily flow, or simply stated, the maximum daily flow will exceed the capacity of the existing effluent pumps.

Table 3.4 provides the estimated operating costs, all costs are represented in 2017-Dollars.

Table 3.4: Estimated Operating Costs

Description	Option 3	Option 9
Average Yearly Operating Cost	\$68,000	\$50,000

Rounded to nearest 000

3.3 Net Present Value Analysis (NPV)

To provide a complete financial analysis, ISL undertook a 50 year Net Present Value analysis using the following basis

- A discount rate of 4%; and
- An inflation rate on the annual operating costs of 2% per year.

Table 3.5: Net Present Value Analysis of Options 1, 2 and 3

Description	Option 3	Option 9
NPV - 50 yrs., 4% Discount Rate, 2% Inflation on	\$53,637,000	\$48,312,000
Operating Costs per year	\$55,657,000	φ46,312,000

Rounded to nearest 000

3.4 Financial Analysis Evaluation

Table 3.6 summarizes the capital costs, operating costs and the net present value analysis over 50 years for all options. Detailed cost estimates and breakdown are included in Appendix A. Total capital costs includes 40% engineering and construction contingencies.



Table 3.6: Capital and Operating Costs and NPV analysis

Description	Option 3	Option 9
Phase 1 - 2017 Construction	\$15,489,000	\$12,327,000
Phase 2 - 2024 Construction	\$6,610,000	\$6,610,000
Phase 3 - (varies)	\$46,983,000	\$44,520,000
Total Capital Costs	\$69,082,000	\$63,457,000
Estimated yearly average operating costs	\$68,000	\$50,000
NPV	\$53,637,000	\$48,312,000

Option 9 represents a lower capital and operational cost over 50 years compared with Option 3.

4.0 Advantages and Disadvantages

The advantages and disadvantages of Option 9 are summarized in Table 3.7. Option 3 is included for comparison purposes.

Table 3.7: Option 3 and 9 Advantages and Disadvantages

Option #	Advantages	Disadvantages
Option 3	 The whole plant effluent flow will be less than 10 mg/L TSS on a consistent base Provide a physical barrier for the whole effluent flow Easier to construct UV disinfection is more efficient and lower operating cost for the UV may be achieved. The saving cannot be determined at this time without pilot testing Minimum disturbance to the current operation during construction Less disturbance to electrical feed system during construction Superior effluent quality will provide the CVRD with future proofing should the TSS regulations be tightened 	Higher capital and operating cost compared with Option 9
Option 9	The portion of the effluent that will be used for effluent reuse will be less than 10 mg/L TSS on a consistent base	 Less efficient for UV disinfection compared with Option 3 Does not provide a physical barrier for effluent Difficult to construct due to flow splitting and more yard piping More disturbance to the current operation during construction compared with Option 3. The Option require flow splitting to the shallow clarifiers in area congested with existing pipes.

5.0 Recommendation

Memorandum



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Both Options are viable options and can be incorporated in the existing treatment plant. Option 3 is more expensive approximately \$69M versus \$63.5M for Option 9. The difference in capital cost is approximately \$5.5M, with approximately \$3.1M by year 2017 and \$2.4 by year 2034. Also, the yearly operating costs for Option 9 is \$50.0 K which is less than Option 3 (\$68.0 K).

Yearly Operating costs for Options 3 and 9 are estimated at \$68.0 K and \$50.0 K respectively. These operating costs do not include the electrical power cost for the new UV system. AECOM UV Disinfection Feasibility Study, 2016, estimated the electrical power cost at \$30.1 K and \$43.0 K for year-1 and year-25 respectively. These power costs are based on achieving 200 MPN/100 mL (fecal coliform counts) and without incorporating cloth media filters. As indicated in AECOM study, applying effluent filtration will reduce the required UV dose which will reduce the yearly operating costs for the UV system.

At the same time, UV systems require chemical cleaning to keep lamps clean during operation. Cloth media filters produce better effluent quality which reduces the frequency of chemical cleaning. The cost of chemical cleaning (labour and material) is not included in the estimated operating costs. These savings are not captured in the operating costs and are difficult to estimate without proper pilot testing. ISL believes that the difference in the operating costs for Options 3 and 9 (\$18.0 K) can be easily captured, as a result of incorporating the cloth media filters within the existing treatment plant which will provide more efficient operation of the UV disinfection process.

Based on the advancements of filtration technology, Option 3 provides some technical advantages over Option 9 which include better effluent quality and truly physical barrier for the effluent which assure that the plant will not exceed its TSS effluent limits and will provide the CVRD with future proofing should the TSS regulations be tightened. Option 3 provides a better effluent quality for UV disinfection. The option is easy to construct with a minimal disturbance to the current operation of the treatment plant.

Please do not hesitate to call if you require addition information.

Regards

Ashraf Rayyan, M.Eng., P.Eng., PMP Manager, Water and Wastewater

Appendix AFinancial Analysis

Title CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase I

Date

26-Jun-16

Description

Year Replace existing 12 mm mechanical screen with 6 mm screen 2017 Add grit removal tank c/w cyclones and classifiers units 2017 Decommissioning of existing primary sludge cyclones and classifiers 2017 and send the primary sludge directly to the sludge thickeners • Injecting polymers prior cloth media filters (provision to be confirmed 2017 by pilot testing)

Add fourth clarifier 2017 Construct offline equalization tank 2017 Repair of existing offshore pipe

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Capital Cost Estimate

			Material	or Eq	uipment Co	st			abor /	Total Line Item	Total Item Cost
ltem	Description	Unit	Quantity	Uni	it Price (\$)	Aı	mount (\$)		allation sts (\$)	Cost (\$)	(\$)
.0 N	Mechanical Screen										\$ 452,000
1.1	General Requirements										\$91,00
	General requirement includes (overhead, indirect cost,										
	2.1.1 contractor profit, mobilization and demobilization and									\$ 91,000	
	temporary work at 25% of project value)										
1.2	Process Mechanical										\$316,00
	1.2.1 Mechanical Screen c/w Washer and Compactor	L.S.	1	\$	212,000	\$	212,000	\$	48,000	\$ 260,000	
	1.2.2 Sluice Gates	unit	1	\$	50,000	\$	50,000	\$	6,000	\$ 56,000	
1.3	Electrical						•		·		\$45,00
	1.3.1 Motor Controls	Motors	1	\$	20,000	\$	20,000	\$	-	\$ 20,000	· ,
	1.3.2 Instruments and Control	L.S.	1	\$	20,000	\$	20,000	\$	-	\$ 20,000	
	1.3.3 Integration	L.S.	1	\$	5,000		5,000		-	\$ 5,000	
o G	Grit Removal				-,		2,222	·		, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	\$ 1,025,00
2.1	General Requirements										\$205,00
	General requirement includes (overhead, indirect cost,										
	2.1.1 contractor profit, mobilization and demobilization and									\$ 205,000	
	temporary work at 25% of project value)										
2.2	Site Civil, Access Road, and Landscaping							\$		I	\$119,00
=	Cita Classing/ Stripping and Stackpile (Area of shamber plus	s			_						1
	2.2.1 Site Clearing/ Stripping and Stockpile (Area of chamber plus 10m, perimeter)	sq.m.	225	\$	5	\$	1,125	\$	-	\$ 1,125	
	2.2.2 Chamber Excavation and Backfilling	cu.m.	1,170	\$	15	\$	17,550	\$	_	\$ 17,550	
	2.2.3 Inter-connecting Pipe Below Grade Pipework	li.m.	50	\$	2,000	\$	100,000	\$	_	\$ 100,000	
2.3	Process Mechanical	,		ΙΨ	2,000	Ψ	100,000	Ψ		ψ 100,000	\$480,00
	2.3.1 Grit Removal Equipment	L.S.	1	\$	300,000	\$	300,000	\$	48,000	\$ 348,000	
	2.3.2 Sluice Gates	unit	2	\$	50,000	\$	100,000	\$	12,000	\$ 112,000	
	2.3.3 Connection to existing Odor System	L.S.	1	\$	10,000		10,000	T	-	\$ 10,000	
	2.3.4 Weirs for splitter box	L.S.	<u>.</u> 1	\$	10,000		10,000			\$ 10,000	
2.4	Structural		•	Ψ	10,000	Ψ	10,000	Ψ		φ 10,000	\$146,00
	2.4.1 Concentrator and Channels Walls	cu.m.	44	\$	1,500	\$	66,007	\$		\$ 66,007	Ψ140,00
	2.4.2 Bottom Slab for Concentrator and Channel	cu.m.	22	\$	1,100	\$	24,241			\$ 24,241	
	2.4.3 Top Slab for Concentrator	cu.m.	19	\$	1,500	\$	27,778	\$	_	\$ 27,778	
	2.4.4 Concrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000	\$	20,000	\$		\$ 20,000	
	2.4.5 Handrail (Install Inc.)	li.m	16	\$	150	\$	2,356			\$ 2,356	
	2.4.6 Access Road and Parking Pad	L.S.	10	\$	5,000	\$	5,000	\$		\$ 5,000	
2.5	Electrical	L.J.	<u> </u>	Ψ	3,000	φ	3,000	φ		φ 5,000	\$65.00
	2.5.1 Motor Controls	Motors	2	\$	20,000	\$	40,000	\$		\$ 40,000	φυσ,υι
	2.5.2 Instruments and Control	L.S.	1	\$	20,000	\$	20,000	<u>φ</u> \$		\$ 20,000	
	2.5.2 Institutions and Control	L.S.	1	\$	5,000	\$	5,000	\$		\$ 20,000	
) e		L.S.	I	Ф	5,000	Ф	5,000	Ф		φ 5,000	\$10,00
2.6	Decommissioning		1	•	10.000	ď	10.000	Φ.		e 10.000	\$10,00
	2.6.1 Grit Removal Equipment	L.S.	7	\$	10,000	\$	10,000	\$	-	\$ 10,000	

2017

Title CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase I

Date

26-Jun-16

Description Replace existing 12 mm mechanical screen with 6 mm screen

2017 Add grit removal tank c/w cyclones and classifiers units 2017

Decommissioning of existing primary sludge cyclones and classifiers 2017 and send the primary sludge directly to the sludge thickeners

 Injecting polymers prior cloth media filters (provision to be confirmed by pilot testing)
 Add fourth clarifier 2017 2017

 Construct offline equalization tank 2017

 Repair of existing offshore pipe 2017 **Additional Notes**

Installation included unless otherwise stated

Items not included

Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Capital Cost Estimate

		5		Material	or E	quipment Co	st			abor /	Tota	al Line Item	Total Item Cost
Item		Description	Unit	Quantity	Ui	nit Price (\$)	Aı	mount (\$)		allation sts (\$)	•	Cost (\$)	(\$)
	ourth C												\$ 2,167,000
3.1		al Requirements											\$434,000
		General requirement includes (overhead, indirect cost,											
		contractor profit, mobilization and demobilization and									\$	434,000	
		temporary work at 25% of project value)											
3.2		vil, Access Road, and Landscaping							\$	-			\$304,000
		Site Clearing/ Stripping and Stockpile (Area of tank plus 10m,	sq.m.	700	\$	5	\$	3,500	\$	_	\$	3,500	
		perimeter)	·			-					•	<u> </u>	
	3.2.2	RAS and WAS piping	L.S.				\$	200,000	\$	-	\$	200,000	
		Relocating utilities at Clarifier location	L.S.				\$	100,000	\$	-	\$	100,000	****
3.3		s Mechanical Clarifier Mechanism	L.S.	4	Τ.	F00 000	Φ.	506,000	œ.	100.000	r.	686,000	\$998,000
			L.S.	1 1	\$	506,000	\$	100,000		180,000	\$		
		Polymer injection system (provision) RAS/WAS Valves and Pipes	L.S.	1	\$	100,000 200,000		200,000		12,000	\$	112,000 200,000	
3.4	Structu		L.S.	<u> </u>	Ф	200,000	Φ	200,000	Ф	-	φ	200,000	\$392,000
3.4		Clarifier Walls	cu.m.	157	\$	1,500	\$	235,242	Ф	_	\$	235,242	\$392,000
		Bottom Slab for Clarifier Tank	cu.m.	30	\$	1,100	\$	33,175		-	\$	33,175	
		Access Stairs	cu.m.	8	\$	1,500		11,310		-	\$	11,310	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$	50,000		-	\$	50,000	
		Handrail (Install Inc.)	li.m	75	\$	150		11,310		_	\$	11,310	
		Splitter box provision	L.S.	1	\$	50,000	\$	50,000		_	\$	50,000	
3.5	Electric		<u> </u>		Ψ	00,000	Ψ	00,000	Ψ		Ψ	00,000	\$40,000
0.0		Motor Controls	Motors	1	\$	10,000	\$	10,000	\$	-	\$	10,000	Ψ+0,000
		Instruments and Controls	L.S.	1	\$	20,000		20,000		-	\$	20,000	
		Integration	L.S.	1	\$	10,000		10,000		-	\$	10,000	
4.0 E		Filtration Package	2.0.		1 4	. 0,000	Ť	. 0,000	<u> </u>		Ť		\$ 863,000
		al Requirements											\$173,000
		General requirement includes (overhead, indirect cost,											, .,
	4.1.1	contractor profit, mobilization and demobilization and									\$	173,000	
		temporary work at 25% of project value)										•	
4.2		vil, Access Road, and Landscaping							\$	-			\$50,000
	4.2.1	Pipes for cloth media filter to the headwork	L.S.				\$	50,000	\$	-	\$	50,000	·
4.3		s Mechanical											\$450,000
	4.3.1	Effluent filteration package	L.S.	1	\$	250,000	\$	250,000	\$	80,000	\$	330,000	
	4.3.2	Effluent reuse valves and pipes	L.S.	1	\$	120,000	\$	120,000	\$	-	\$	120,000	
4.4	Structu	ıral											\$120,000
	4.4.1	Increase in the UV building to accommodate cloth media filter	L.S.	1	\$	120,000	\$	120,000	\$	-	\$	120,000	
4.5	Electric												\$70,000
		Motor Controls	Motors	4	\$	10,000	\$	40,000		-	\$	40,000	
	4.5.2	Instruments and Controls	L.S.	1	\$	20,000	\$	20,000		-	\$	20,000	
	4.5.3	Integration	L.S.	1	\$	10,000	\$	10,000	\$	-	\$	10,000	

Year

Concept Design Cost Estimate for Option 9 - Phase I

Date

26-Jun-16

Description Replace existing 12 mm mechanical screen with 6 mm screen

Add grit removal tank c/w cyclones and classifiers units

Decommissioning of existing primary sludge cyclones and classifiers and send the primary sludge directly to the sludge thickeners 2017

 Injecting polymers prior cloth media filters (provision to be confirmed by pilot testing)
 Add fourth clarifier 2017

2017 Construct offline equalization tank 2017

 Repair of existing offshore pipe 2017 **Additional Notes**

Installation included unless otherwise stated

Items not included

Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Capital Cost Estimate

		5 1.0	Material or Equipment Cost Description		_	Labor /	Total Line Item	Total Item Cost				
Item		Description	Unit	Quantity	Un	it Price (\$)	A	mount (\$)	١	nstallation Costs (\$)	Cost (\$)	(\$)
5.0 C	offline E	qualization Tank										\$ 4,177,000
5.1	Genera	al Requirements										\$836,000
		General requirement includes (overhead, indirect cost,										
	5.1.1	contractor profit, mobilization and demobilization and									\$ 836,000	
		temporary work at 25% of project value)										
5.2	Site Ci	vil, Access Road, and Landscaping							\$	-		\$322,000
	5.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	3,025	\$	5	\$	15,125	\$	-	\$ 15,125	
	5.2.2	Tank Excavation and Backfilling	cu.m.	15,125	\$	15	\$	226,875	\$	-	\$ 226,875	
	5.2.3	Inter-connecting Pipe Below Grade Pipework	li.m.	40	\$	2,000	\$	80,000	\$	-	\$ 80,000	
5.3		s Mechanical										\$1,182,000
	5.3.1	Equalization Pumps	unit	2	\$	60,000	\$	120,000	\$		\$ 165,000	
		Gates	unit	2	\$	50,000		100,000		12,000		
		Connection to existing Odor System	li.m.	200	\$	1,000		200,000		-	\$ 200,000	
	5.3.4	Pumps Pipes and Valves	L.S.	1	\$	180,000		180,000	\$	-	\$ 180,000	
	5.3.5	Mixing mixers	unit	8	\$	60,000	\$	480,000	\$	45,000	\$ 525,000	
5.4	Structu											\$1,632,000
		Tank Walls	cu.m.	336	\$	1,500		504,000		-	\$ 504,000	
		Bottom Slab for Tank	cu.m.	613	\$	1,100		673,750	\$	-	\$ 673,750	
		Top Slab for Tank	cu.m.	368	\$	1,100		404,250	\$	-	\$ 404,250	
		Mis. Metals	L.S.	1	\$	30,000		30,000		-	\$ 30,000	
		Access Road and Parking Pad	L.S.	1	\$	20,000	\$	20,000	\$	-	\$ 20,000	
5.5	Electric											\$205,000
		Motor Controls	Motors	8	\$	20,000		160,000		-	\$ 160,000	
		Instruments and control	L.S.	1	\$	40,000		40,000		-	\$ 40,000	
		Integration	L.S.	1	\$	5,000	\$	5,000	\$	-	\$ 5,000	
		f existing outfall pipe			_		,					\$ 120,000
6.1		al Requirements										\$0
		Included in outfall sections costs									\$ -	
6.2		of existing outfall pipe	,		,						T	\$120,000
	6.2.1	Repair of existing outfall pipe	L.S.	1	\$	120,000	\$	120,000	\$	-	\$ 120,000	
		Total Capital Cost										\$8,805,000

Year

2017

2017

Title

CVWPCC WWTF
Concept Design Cost Estimate for Option 9 - Phase 2

Date

26-Jun-16

Description

Construct one aeration tank and clarifier

Year 2024

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes
UV disinfection

				Material	or Eq	uipment Co	st		Labour /	Total Line Iten	n Total Item Cost
Item		Description	Unit	Quantity	Un	it Price (\$)	Am	ount (\$)	Installation Costs (\$)	Cost (\$)	(\$)
1.0 A	eration	Tank & Clarifier	<u>' </u>								\$ 4,720,000
1.1	Genera	al Requirements									\$944,00
		General requirement includes (overhead, indirect cost,									
	1.1.1	contractor profit, mobilization and demobilization and								\$ 944,000)
		temporary work at 25% of project value)									
1.2	Site Ci	vil, Access Road, and Landscaping							\$ -		\$714,00
	1.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m,	00 m	2,725	\$	5	¢	13,625	\$ -	\$ 13,625	
	1.2.1	perimeter)	sq.m.	2,725	Ф	э	\$	13,023	Ф -	φ 13,023	·
	1.2.2	Access Road and Parking Pad	L.S.	1	\$	100,000	\$	100,000	\$ -	\$ 100,000)
	1.2.3	Inter-connecting Pipes Below Grade Pipework (from primary	li.m.	250	\$	1,500	\$	375,000	\$ -	\$ 375,000	
	1.2.3	splitter to aeration tank)	11.111.	230	Ψ	1,500	Ψ	373,000	φ -	φ 3/3,000	'
		RAS and WAS piping	li.m.	50	\$	1,500	\$	75,000	\$ -	\$ 75,000	
	1.2.5	Air piping	li.m.	100	\$	1,500	\$	150,000	\$ -	\$ 150,000)
1.3	Proces	ss Mechanical									\$1,670,00
	1.3.1	Fine bubble diffusers and air pipes	L.S.	1	\$	280,000	\$	280,000	\$ 180,000	\$ 460,000	
		Mixer	unit	1	\$	60,000		60,000	\$ 12,000	\$ 72,000)
		Clarifier Mechanism	L.S.	1	\$	506,000	\$	506,000	\$ 180,000	\$ 686,000	
		RAS/WAS pumping	unit	4	\$	60,000	\$		\$ 12,000		
	1.3.5	RAS/WAS Valves and Pipes	L.S.	1	\$	200,000	\$	200,000	\$ -	\$ 200,000	
1.4	Structu										\$1,161,00
		Aeration Tank Walls	cu.m.	313	\$	1,500	\$	468,750		\$ 468,750	
		Bottom Slab for Aeration Tank	cu.m.	260	\$	1,100	\$	286,000		\$ 286,000	
	1.4.3	Access stairs	cu.m.	26	\$	1,500	\$	39,000	\$ -	\$ 39,000)
	1.4.4	Handrail (Install Inc.)	li.m	170	\$	150	\$	25,500		\$ 25,500	
		Clarifier Walls	cu.m.	157	\$	1,500	\$	235,242		\$ 235,242	
		Bottom Slab for Clarifier Tank	cu.m.	30	\$	1,100	\$	33,175	\$ -	\$ 33,175	5
		Access Stairs	cu.m.	8	\$	1,500	\$	11,310	\$ -	\$ 11,310)
	1.4.8	Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$	50,000		\$ 50,000	
	1.4.9	Handrail (Install Inc.)	li.m	75	\$	150	\$	11,310	\$ -	\$ 11,310)
1.5	Plumb										\$50,00
	1.5.1	Plumbing	L.S.	1	\$	50,000	\$	50,000	\$ -	\$ 50,000)
1.6	Electri	cal									\$182,00
	1.6.1	Motor Controls	Motors	4	\$	10,000	\$	40,000	\$ -	\$ 40,000)
		Instruments and Controls	L.S.	1	\$	130,000	\$	130,000	\$ -	\$ 130,000	
	1.6.3	Integration	L.S.	1	\$	12,000	\$	12,000	\$ -	\$ 12,000	
		Total Capital Cost									\$4,721,00

Title 31548 CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase 3

Date

26-Jun-16

 Description
 Year

 ● Replace all outfall sections (onshore/offshore)
 2031

Construct two primary clarifiers and process building
 Upgrade cloth media filter
 Upgrade effluent pumps
 2034

Add mechanical screens to new process building
 Add grit removal tank c/w cyclones and classifiers units
 Construct new thickener
 2045

Install new centrifuge
 Construct one aeration tank and clarifier
 2060

Capital Cost Estimate

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes
UV disinfection

lt o m		Decayintian		Material	or Ec	quipment Co	st		l.	Labor / stallation	To	tal Line Item	Total Item Cost
Item		Description	Unit	Quantity	Ur	nit Price (\$)	Α	mount (\$)		Stallation Costs (\$)		Cost (\$)	(\$)
		Outfall Sections (Onshore/Offshore) - Year (2031)											\$ 14,109,000
1.1		al Requirements											\$
	1.1.1	Included in outfall sections costs									\$	-	
1.2	Civil								\$	-			\$13,949,00
		900 mm Tie-In and temporary works	L.S.	11	\$	40,000			\$	-	\$	40,000	
		Onshore Section (2827.0 m Length)	L.S.	1	\$	7,633,000		7,633,000		-	\$	7,633,000	
		Offshore section (2825.0 m Length)	L.S.	1	\$	6,215,000		6,215,000		-	\$	6,215,000	
		Diffuser section (175.0 m Length)	L.S.	1	\$	61,000	\$	61,000	\$	-	\$	61,000	
1.3		nical and Electrical											\$160,00
	1.3.1	Add fourth pump	L.S.	1	\$	150,000		150,000		-	\$	150,000	
	1.3.2	Integration	L.S.	1	\$	10,000	\$	10,000	\$	-	\$	10,000	
		Clarifiers + Process Building - Year (2033)											\$ 7,650,000
2.1	Genera	al Requirements					,						\$1,530,00
		General requirement includes (overhead, indirect cost,											
		contractor profit, mobilization and demobilization and									\$	1,530,000	
		temporary work at 25% of project value)											
2.2	Site Civ	vil, Access Road, and Landscaping					,		\$	-			\$219,00
		Site Clearing/ Stripping and Stockpile (Area of building and	sq.m.	3,687	\$	5	\$	18,435	\$	_	\$	18.435	
		tank plus 10m, perimeter)	·	•			,	•	•			-,	
		Access Road and Parking Pad	L.S.	1	\$	200,000	\$	200,000	\$	-	\$	200,000	
2.3		s Mechanical	1										\$2,568,00
	2.3.1	Primary Clarifier Mechanism	L.S.	2	\$	360,000		720,000		180,000		900,000	
		Air Blowers	L.S.	5	\$	150,000		750,000		180,000		930,000	
		WAS pumping	unit	2	\$	60,000		120,000		12,000		132,000	
		WAS Valves and Pipes	L.S.	1	\$	150,000		150,000		-	\$	150,000	
		Air Valves and Pipes	L.S.	1	\$	250,000	\$	250,000	\$	-	\$	250,000	
		Sluice Gates	unit	4	\$	50,000	\$	200,000	\$	6,000	\$	206,000	
2.4	Structu		1										\$2,402,00
	2.4.1	Primary Tank Walls	cu.m.	150	\$	1,500		225,000	\$	-	\$	225,000	
		Bottom Slab for Primary Tank	cu.m.	160	\$	1,100		176,000	\$	-	\$	176,000	
		Access stairs	cu.m.	16	\$	1,500				-	\$	24,000	
		Process Building	cu.m.	250	\$	1,500			\$	-	\$	375,000	
		Bottom Slab for Process Building	cu.m.	216	\$	1,100			\$	-	\$	237,600	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	150,000			\$	-	\$	150,000	
		Handrail (Install Inc.)	li.m	170	\$	150	\$	25,500	\$	-	\$	25,500	
		Superstructure + Architectural (Process Building, 6 m tall,	sq.m.	540	\$	2,200	\$	1,188,000	\$	_	\$	1,188,000	
		steel frame with masonry infill)	Jq.111.	040	Ψ	2,200	Ψ	1,100,000	Ψ		Ψ	1,100,000	
2.5		ing & HVAC											\$800,00
		Plumbing	L.S.	1	\$	300,000		300,000		-	\$	300,000	
		HVAC	L.S.	1	\$	500,000	\$	500,000	\$	-	\$	500,000	
2.6	Electric		1										\$132,00
		Motor Controls	Motors	4	\$	10,000		40,000		-	\$	40,000	
		Instruments and Controls	L.S.	1	\$	80,000		80,000		-	\$	80,000	
	2.6.3	Integration	L.S.	1	\$	12,000	\$	12,000	\$	-	\$	12,000	

Title 31548 CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase 3

Date

26-Jun-16

Year Description Replace all outfall sections (onshore/offshore) 2031

> Construct two primary clarifiers and process building 2033 Upgrade cloth media filter 2034 Upgrade effluent pumps 2043 Add mechanical screens to new process building

> 2045 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056 Install new centrifuge 2060

Construct one aeration tank and clarifier

2063

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs

Contingency Allowances Taxes

UV disinfection

Material or Equipment Cost Cost (\$)	Capita	I Cost E	Estimate		Matarial	or E	www.mant.Co	o t		Labo	r /			
Solid Middle Cloth Filter (2034) Solid Middle C	Item		Description		Materiai	or E	quipment Co	St					Tota	
3.1 General Requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value) \$ 352,000 \$ 352,000 \$ 3.2 Contractor profit, mobilization and demobilization and demobilizatio			23330,	Unit	Quantity	Uı	nit Price (\$)	Α	mount (\$)			Cost (\$)		(\$)
Seneral requirement includes (overhead, indirect cost, 3.1 contractor profit, mobilization and demobilization and temporary work at 25% of project value) \$1,322,000 \$3.2 Process Mechanical \$30,000 \$ 30,000 \$ 12,000 \$ 42,000 \$1,322,000 \$3.2.2 [Cloth media filter equipment unit 1	3.0 M	edia Clo	oth Filter (2034)										\$	1,759,000
3.1 contractor profit, mobilization and demobilization and lemporary work at 25% of project value)	3.1	Genera	I Requirements											\$352,000
Itemporary work at 25% of project value)														
3.2 Process Mechanical												\$ 352,000		
3.2.2 Cloth media filter equipment	3.2													\$1,322,000
3.2.3 Pipes and Valves L.S. 1		3.2.1	Modification to Polymer Injection System	unit	1				,					
3.3 Electrical Motor Controls Motors 2 \$ 20,000 \$ 40,000 \$ - \$ \$ 40,000 \$					1						0,000			
3.3.1 Motor Controls		3.2.3	Pipes and Valves	L.S.	1	\$	50,000	\$	50,000	\$	-	\$ 50,000		
3.3.2 Instruments and Control L.S. 1	3.3	Electric	cal											\$85,000
3.3.3 Integration		3.3.1	Motor Controls	Motors	2						-	.,		
4.1 General Requirements \$ 1,780,000		3.3.2	Instruments and Control	L.S.	1	\$	40,000	\$	40,000	\$	-	\$ 40,000		
4.1 General Requirements \$0 4.1.1 Included in effluent pumps item costs \$ 4.1.1 Included in effluent pumps item costs \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000 \$ 50,000				L.S.	1	\$	5,000	\$	5,000	\$	-	\$ 5,000		
4.1.1 Included in effluent pumps item costs \$ -	4.0 E	ffluent F	Pumps - Year (2043)										\$	1,780,000
4.2 Site Civil, Access Road, and Landscaping	4.1	Genera	I Requirements											\$0
4.2.1 Interconnecting pipes within CVWPCC		4.1.1	Included in effluent pumps item costs									\$ -		
4.3 Replace existing pumps	4.2	Site Civ	vil, Access Road, and Landscaping											\$50,000
4.3.1 Replace existing pumps		4.2.1	Interconnecting pipes within CVWPCC	L.S.	1	\$	50,000	\$	50,000	\$	-	\$ 50,000		
4.3.2 Valves and pipes (within the vault)	4.3													\$1,200,000
4.4 Structural		4.3.1	Replace existing pumps	L.S.	1						-			
4.4.1 New outfall chamber		4.3.2	Valves and pipes (within the vault)	L.S.	1	\$	600,000	\$	600,000	\$	-	\$ 600,000		
4.5 Electrical	4.4	Structu	ıral											\$80,000
4.5.1 Electrical L.S. 1 \$ 370,000 \$ 370,000 \$ - \$ 370,000 \$ 4.5.2 Instruments and control L.S. 1 \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000 \$ - \$ 80,000		4.4.1	New outfall chamber	L.S.	1	\$	80,000	\$	80,000	\$	-	\$ 80,000		
4.5.2 Instruments and control L.S. 1 \$ 80,000 \$ 80,000 \$ - \$ 80,000	4.5	Electric	cal											\$450,000
5.0 Mechanical Screen - Year (2045) \$892,000 5.1 General Requirements \$179,000 5.1.1 contractor profit, mobilization and demobilization and temporary work at 25% of project value) \$179,000 5.2 Process Mechanical \$648,000 5.2.1 Mechanical Screen c/w Washer and Compactor L.S. 2 \$300,000 \$600,000 \$48,000 \$648,000 5.3 Electrical \$65,000 5.3.1 Motor Controls Motors 2 \$20,000 \$40,000 - \$40,000 5.3.2 Instruments and control L.S. 1 \$20,000 20,000 - \$20,000		4.5.1	Electrical	L.S.	1	\$	370,000	\$			-	\$ 370,000		
S.1 General Requirements General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value) S.2 Process Mechanical S.2.1 Mechanical Screen c/w Washer and Compactor L.S. 2 \$300,000 \$600,000 \$48,000 \$648,000 \$5.3.1 Motor Controls S.3.1 Motor Controls Motors 2 \$20,000 \$40,000 \$- \$40,000 \$5.3.2 Instruments and control L.S. 1 \$20,000 \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$- \$20,000 \$-		4.5.2	Instruments and control	L.S.	1	\$	80,000	\$	80,000	\$	-	\$ 80,000		
Separate General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value) \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000 \$ 179,000	5.0 M	echanic	cal Screen - Year (2045)										\$	892,000
5.1.1 contractor profit, mobilization and demobilization and temporary work at 25% of project value) 5.2 Process Mechanical	5.1	Genera	I Requirements											\$179,000
temporary work at 25% of project value)			General requirement includes (overhead, indirect cost,											
5.2 Process Mechanical		5.1.1	contractor profit, mobilization and demobilization and									\$ 179,000		
5.2 Process Mechanical			temporary work at 25% of project value)											
5.3 Electrical 5.3.1 Motor Controls Motors 2 \$ 20,000 \$ 40,000 \$ - \$ 40,000 5.3.2 Instruments and control L.S. 1 \$ 20,000 \$ - \$ 20,000	5.2					-		-	•			•	•	\$648,000
5.3 Electrical 5.3.1 Motor Controls Motors 2 \$ 20,000 \$ 40,000 \$ - \$ 40,000 5.3.2 Instruments and control L.S. 1 \$ 20,000 \$ - \$ 20,000		5.2.1	Mechanical Screen c/w Washer and Compactor	L.S.	2	\$	300,000	\$	600,000	\$ 4	8,000	\$ 648,000		
5.3.2 Instruments and control L.S. 1 \$ 20,000 \$ - \$ 20,000	5.3						-						•	\$65,000
5.3.2 Instruments and control L.S. 1 \$ 20,000 \$ - \$ 20,000		5.3.1	Motor Controls	Motors	2	\$	20,000	\$			-	\$ 40,000		
		5.3.2	Instruments and control		1	\$	20,000	\$	20,000	\$	-	\$ 20,000		
				L.S.	1	\$	5,000	\$	5,000	\$	-	\$ 5,000		

Title 31548 CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase 3

Date

26-Jun-16

Description Year Replace all outfall sections (onshore/offshore) 2031

7.4.4 Concrete Walkways / Access Ramp / Road

 Construct two primary clarifiers and process building 2033 Upgrade cloth media filter 2034 Upgrade effluent pumps 2043

 Add mechanical screens to new process building 2045 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056

 Install new centrifuge 2060 Construct one aeration tank and clarifier 2063

Capital Cost Estimate

		.		Material	or E	quipment Co	st			Labor /	Tot	al Line Item	Total Item Cost
Item		Description	Unit	Quantity	U	nit Price (\$)	Aı	mount (\$)		stallation Costs (\$)	\$ 203,000 - \$ 1,129 - \$ 1,7550 - \$ 100,000 - \$ 10,000 - \$ 10,000 - \$ 10,000 - \$ 24,24 - \$ 27,776 - \$ 20,000 - \$ 2,356 - \$ 5,000 - \$ 40,000 - \$ 5,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000 - \$ 40,000		(\$)
6.0 G	rit Rem	oval - Year (2045)											\$ 1,013,000
6.1	Genera	al Requirements											\$203,000
		General requirement includes (overhead, indirect cost,											
	6.1.1	contractor profit, mobilization and demobilization and									\$	203,000	
		temporary work at 25% of project value)											
6.2	Site Ci	vil, Access Road, and Landscaping	1 1						\$	-			\$119,000
l	6.2.1	Site Clearing/ Stripping and Stockpile (Area of chamber plus	sq.m.	225	\$	5	\$	1,125	\$	-	\$	1,125	
		10m, perimeter) Chamber Excavation and Backfilling		4.470		45						•	
			cu.m.	1,170 50	\$	15	,	17,550					
6.3		Inter-connecting Pipe Below Grade Pipework s Mechanical	li.m.	50	\$	2,000	Ъ	100,000	Ф	<u>-</u>	Ф	100,000	\$480,000
0.3		Grit Removal Equipment	L.S.	1	\$	300,000	\$	300,000	Ф	48 000	Ф	348 000	\$400,000
		Sluice Gates	unit	2	\$	50,000		100,000					
		Connection to existing Odor System	L.S.	1	\$	10,000		10,000		12,000			
		Weirs for splitter box	L.S.	1	\$	10,000		10,000			•		
6.4	Structi		L.O.	'	ļΨ	10,000	ļΨ	10,000	Ψ		Ψ	10,000	\$146,000
		Concentrator and Channels Walls	cu.m.	44	\$	1,500	\$	66,007	\$	_	\$	66.007	ψ. 10,000
		Bottom Slab for Concentrator and Channel	cu.m.	22	\$	1,100		24,241		_	•	24,241	
		Top Slab for Concentrator	cu.m.	19	\$	1,500		27,778		-		27,778	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000		20,000		-	_	20,000	
		Handrail (Install Inc.)	li.m	16	\$	150	\$	2,356	\$	-	\$	2,356	
		Access Road and Parking Pad	L.S.	1	\$	5,000	\$	5,000		-	\$	5,000	
6.5	Electri	cal	•										\$65,000
		Motor Controls	Motors	2	\$	20,000		40,000		-	\$	40,000	
		Instruments and control	L.S.	1	\$	20,000	\$	20,000		-	\$	20,000	
		Integration	L.S.	1	\$	5,000	\$	5,000	\$	-	\$	5,000	
7.0 T		er - Year (2056)											\$ 1,072,000
7.1	Genera	al Requirements											\$215,000
		General requirement includes (overhead, indirect cost,											
	7.1.1	contractor profit, mobilization and demobilization and									\$	215,000	
		temporary work at 25% of project value)	ļl				<u> </u>						****
7.2	Site Ci	vil, Access Road, and Landscaping	1 1		_				\$	-			\$144,000
	7.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	800	\$	5	·	4,000	\$	-	\$	4,000	
		Access Road and Parking Pad	L.S.	1	\$	40,000		40,000		-		40,000	
		Inter-connecting Pipes Below Grade Pipework	L.S.	1	\$	100,000	\$	100,000	\$	-	\$	100,000	
7.3		s Mechanical											\$480,000
		Thickener Mechanism	L.S.	1	\$	250,000		250,000	\$	180,000	_	430,000	
		Connection to existing Odor System	L.S.	1	\$	50,000	\$	50,000			\$	50,000	
7.4	Structu		, r		1 -		T &		_			1	\$198,000
		Thickener Tank Walls	cu.m.	32	\$	1,500		48,000		-	\$	48,000	
		Bottom Slab for Thickener Tank	cu.m.	63	\$	1,100		69,300		-	\$	69,300	
	7.4.3	Thickener cover	L.S.	1	\$	30,000	\$	30,000	\$	-	\$	30,000	

L.S.

50,000 \$

50,000 \$

50,000

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Title 31548 CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase 3

Date

26-Jun-16

Description Replace all outfall sections (onshore/offshore)

2031 Construct two primary clarifiers and process building 2033 Upgrade cloth media filter 2034

 Upgrade effluent pumps 2043 Add mechanical screens to new process building 2045 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056

 Install new centrifuge 2060 Construct one aeration tank and clarifier 2063

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes UV disinfection

Capital Cost Estimate

		Stimate		Material	or Eq	uipment Co	st		Labor /	Т	Total Line Item	Total Item Cost
Item		Description	Unit	Quantity	Un	it Price (\$)	Α	mount (\$)	Installation Costs (\$)		Cost (\$)	(\$)
7.5	Electric	cal										\$35,000
		Motor Controls	Motors	1	\$	10,000	\$	10,000	\$ -		\$ 10,000	•
	7.5.2	Instruments and Controls	L.S.	1	\$	20,000	\$	20,000	\$ -	5	\$ 20,000	
	7.5.3	Integration	L.S.	1	\$	5,000	\$	5,000	\$ -	5	\$ 5,000	
8.0 C	entrifug	ge - Year (2060)										\$ 1,190,000
8.1		al Requirements										\$238,000
		General requirement includes (overhead, indirect cost,										
		contractor profit, mobilization and demobilization and								5	\$ 238,000	
		temporary work at 25% of project value)										
8.2		vil, Access Road, and Landscaping							\$ -			\$57,000
		Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	1,225	\$	5	\$	6,125	\$ -	5	\$ 6,125	
	8.2.2	Inter-connecting Pipes Below Grade Pipework	L.S.	1	\$	50,000	\$	50,000	\$		\$ 50,000	
8.3	Proces	s Mechanical										\$530,000
		Centrifuge	L.S.	1	\$	350,000	\$	350,000	\$ 180,00	00 5	\$ 530,000	
8.4	Structu											\$330,000
	8.4.1	Centrifuge base based on extending existing structure	cu.m.	60	\$	1,500	\$	90,000	\$ -	5	\$ 90,000	
		Superstructure + Architectural (Chemical Room, 6 m tall, steel frame with masonry infill)	sq.m.	100	\$	2,200	\$	220,000	\$ -	5	\$ 220,000	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000	\$	20,000	\$ -	-	\$ 20.000	
8.5	Electric		L.O.	ı	Ψ	20,000	Ψ	20,000	Ψ -	,	20,000	\$35,000
0.5		Motor Controls	Motors	1	\$	10,000	\$	10,000	\$ -	1	\$ 10,000	ψ33,000
		Instruments and Controls	L.S.	1	\$	20.000		20,000	\$ -	- 5		
		Integration	L.S.	1	\$	5,000		5,000		3		
9.0		on Tank and Clarifier - Year (2063)	L.O.		, v	0,000	Ψ	0,000	Ψ		φ 0,000	\$ 4,252,000
9.1		Il Requirements										\$851,000
		General requirement includes (overhead, indirect cost,										+++++++++++++++++++++++++++++++++++++
		contractor profit, mobilization and demobilization and								5	\$ 851,000	
		temporary work at 25% of project value)									, ,,,,,,	
9.2		vil, Access Road, and Landscaping	1					<u> </u>	\$ -			\$339,000
	0.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	2,725	\$	5	\$	13,625	\$ -	5	\$ 13,625	, ,
		Access Road and Parking Pad	L.S.	1	\$	100,000	\$	100,000	\$ -		\$ 100,000	
		RAS and WAS piping	L.S.	1	\$	75,000					\$ 75,000	
		Air piping	li.m.	100	\$	1,500	\$	150,000	\$ -		\$ 150,000	
9.3		s Mechanical						,	-		, , , , , , , , , , , , , , , , , , , ,	\$1,670,000
	9.3.1	Fine bubble diffusers and air pipes	L.S.	1	\$	280,000	\$	280,000	\$ 180,00	00	\$ 460,000	
	9.3.2		unit	1	\$	60,000						
	9.3.3	Clarifier Mechanism	L.S.	1	\$	506,000		506,000	\$ 180,00			
		RAS/WAS pumping	unit	4	\$	60,000	\$	240,000	\$ 12,00	00 5		
		RAS/WAS Valves and Pipes	L.S.	1	\$	200,000	\$	200,000	\$ -		\$ 200,000	

Year

Title 31548 CVWPCC WWTF

Concept Design Cost Estimate for Option 9 - Phase 3

Date

26-Jun-16

Description

Year Replace all outfall sections (onshore/offshore) 2031 Construct two primary clarifiers and process building 2033 Upgrade cloth media filter 2034 Upgrade effluent pumps 2043 Add mechanical screens to new process building 2045 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056 Install new centrifuge 2060 Construct one aeration tank and clarifier 2063

Additional Notes

Installation included unless otherwise stated

Items not included

Land procurement Costs

Contingency Allowances
Taxes

UV disinfection

				Material	or Eq	uipment Co	st		Labor /	Tota	al Line Item	Total Item Cost
Item		Description	Unit	Quantity	Un	it Price (\$)	Aı	mount (\$)	Installation Costs (\$)		Cost (\$)	(\$)
9.4	Structu	ural										\$1,161,000
	9.4.1	Aeration Tank Walls	cu.m.	313	\$	1,500	\$	468,750	\$ -	\$	468,750	
	9.4.2	Bottom Slab for Aeration Tank	cu.m.	260	\$	1,100	\$	286,000	\$ -	\$	286,000	
	9.4.3	Access stairs	cu.m.	26	\$	1,500	\$	39,000	\$ -	\$	39,000	
	9.4.4	Handrail (Install Inc.)	li.m	170	\$	150	\$	25,500	\$ -	\$	25,500	
	9.4.5	Clarifier Walls	cu.m.	157	\$	1,500	\$	235,242	\$ -	\$	235,242	
	9.4.6	Bottom Slab for Clarifier Tank	cu.m.	30	\$	1,100	\$	33,175	\$ -	\$	33,175	
	9.4.7	Access Stairs	cu.m.	8	\$	1,500	\$	11,310	\$ -	\$	11,310	
	9.4.8	Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$	50,000	\$ -	\$	50,000	
	9.4.9	Handrail (Install Inc.)	li.m	75	\$	150	\$	11,310	\$ -	\$	11,310	
9.5	Plumbi	ing										\$50,000
	9.5.1	Plumbing	L.S.	1	\$	50,000	\$	50,000	\$ -	\$	50,000	
9.6	Electric	cal										\$182,000
	9.6.1	Motor Controls	Motors	4	\$	10,000	\$	40,000	\$ -	\$	40,000	
	9.6.2	Instruments and Controls	L.S.	1	\$	130,000	\$	130,000	\$ -	\$	130,000	
	9.6.3	Integration	L.S.	1	\$	12,000	\$	12,000	\$ -	\$	12,000	
		Total Capital Cost										\$33,718,000

Concept Design Cost Estimate for Option 3 - Phase I

Date

3-Aug-16

Year Description Replace existing 12 mm mechanical screen with 6 mm screen 2017

> Add grit removal tank c/w cyclones and classifiers units 2017

> Decommissioning of existing primary sludge cyclones and classifiers and send the primary sludge directly to the sludge thickeners 2017

> Injecting polymers prior cloth media filters (provision to be confirmed by pilot testing)
> Add cloth media filter 2017

> 2017 Construct offline equalization tank 2017

> Repair of existing offshore pipe 2017

Additional Notes

Installation included unless otherwise stated

Items not included

Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Capital Cost Estimate	Са	pital	Cost	Estimate
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		5		Material	or Eq	uipment Co	st			bor /	То	tal Line Item	Total I	tem Cost
Item		Description	Unit	Quantity	Un	it Price (\$)	Α	mount (\$)		illation sts (\$)		Cost (\$)		(\$)
1.0 M	echanical	Screen											\$	452,000
1.1	General R	Requirements												\$91,000
		eneral requirement includes (overhead, indirect cost,												
		ntractor profit, mobilization and demobilization and									\$	91,000		
		mporary work at 25% of project value)												
1.2		Mechanical												\$316,000
		echanical Screen c/w Washer and Compactor	L.S.	11	\$	212,000		212,000	•	48,000		260,000		
		uice Gates	unit	11	\$	50,000	\$	50,000	\$	6,000	\$	56,000		
1.3	Electrical													\$45,000
		otor Controls	Motors	11	\$	20,000		20,000		-	\$	20,000		
		struments and Control	L.S.	1	\$	20,000		20,000	\$	-	\$	20,000		
	1.3.3 Int		L.S.	11	\$	5,000	\$	5,000	\$	-	\$	5,000		
	rit Remova												\$	1,025,000
2.1		Requirements												\$205,000
		eneral requirement includes (overhead, indirect cost,												
		ntractor profit, mobilization and demobilization and									\$	205,000		
		mporary work at 25% of project value)												
2.2		Access Road, and Landscaping					,		\$	-	,			\$119,000
		te Clearing/ Stripping and Stockpile (Area of chamber plus	sq.m.	225	\$	5	\$	1,125	\$	_	\$	1,125		
	10	m, perimeter)	oq				<u> </u>	-			<u> </u>	·		
		namber Excavation and Backfilling	cu.m.	1,170	\$	15		17,550	\$	-	\$	17,550		
		ter-connecting Pipe Below Grade Pipework	li.m.	50	\$	2,000	\$	100,000	\$	-	\$	100,000		
2.3		Mechanical					,				,			\$480,000
		it Removal Equipment	L.S.	1	\$	300,000		300,000	\$	48,000		348,000		
		uice Gates	unit	2	\$	50,000		100,000	\$	12,000		112,000		
		onnection to existing Odor System	L.S.	1	\$	10,000		10,000	\$	-	\$	10,000		
		eirs for splitter box	L.S.	1	\$	10,000	\$	10,000	\$	-	\$	10,000		
2.4	Structural						,				,			\$146,000
		oncentrator and Channels Walls	cu.m.	44	\$	1,500		66,007	\$	-	\$	66,007		
		ottom Slab for Concentrator and Channel	cu.m.	22	\$	1,100		24,241	\$	-	\$	24,241		
		pp Slab for Concentrator	cu.m.	19	\$	1,500	,	27,778	\$	-	\$	27,778		
		oncrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000	\$	20,000	\$	-	\$	20,000		
		andrail (Install Inc.)	li.m	16	\$	150		2,356		-	\$	2,356		
		ccess Road and Parking Pad	L.S.	1	\$	5,000	\$	5,000	\$	-	\$	5,000		
2.5	Electrical													\$65,000
		otor Controls	Motors	2	\$	20,000		40,000		-	\$	40,000		
		struments and Control	L.S.	1	\$	20,000		20,000	\$	-	\$	20,000		
	2.5.3 Int		L.S.	1	\$	5,000	\$	5,000	\$	-	\$	5,000		
2.6	Decommis		1											\$10,000
	2.6.1 Gr	it Removal Equipment	L.S.	1	\$	10,000	\$	10,000	\$	-	\$	10,000		

Title CVWPCC WWTF

Concept Design Cost Estimate for Option 3 - Phase I

Date

3-Aug-16

Construct offline equalization tank

Repair of existing offshore pipe

Description

Replace existing 12 mm mechanical screen with 6 mm screen
 Add grit removal tank c/w cyclones and classifiers units
 Decommissioning of existing primary sludge cyclones and classifiers and send the primary sludge directly to the sludge thickeners
 Injecting polymers prior cloth media filters (provision to be confirmed by pilot testing)
 Add cloth media filter

Additional Notes

Installation included unless otherwise stated

Items not included

Land procurement Costs Contingency Allowances

Taxes

UV disinfection

Capital Cost Estimate

		Provide for		Material	or E	quipment Co	st		Labor /	Тс	otal Line Item	Total Item Cost
Item		Description	Unit	Quantity	Uı	nit Price (\$)	I	Amount (\$)	Installation Costs (\$)		Cost (\$)	(\$)
3.0 M	edia Clo	oth Filter										\$ 5,289,000
3.1		al Requirements										\$1,058,000
		General requirement includes (overhead, indirect cost,										1
		contractor profit, mobilization and demobilization and								\$	1,058,000	1
		temporary work at 25% of project value)										I
3.2	Site Ci	vil, Access Road, and Landscaping							\$ -			\$208,000
	3.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	2,100	\$	5	\$	10,500	\$ -	\$	10,500	
	3.2.2	Tank Excavation and Backfilling	cu.m.	2,500	\$	15	\$	37,500	\$ -	\$	37,500	
		Inter-connecting Pipe Below Grade Pipework	li.m.	80	\$	2,000	\$	160,000	\$	\$	160,000	
3.3	Proces	s Mechanical										\$2,729,000
		Polymer Injection System	unit	1	\$	100,000		,			112,000	
	3.3.2	Cloth media filter equipment	unit	1	\$	1,575,000	\$		\$ 180,000		1,755,000	I
		Sluice Gates	unit	12	\$	50,000	\$,	\$ 12,000		612,000	
	3.3.4	Pipes and Valves	L.S.	1	\$	250,000	\$	250,000	\$ -	\$	250,000	I
3.4	Structu											\$1,189,000
		Tank Walls	cu.m.	352	\$	1,500				\$	528,000	
		Bottom Slab for Tank	cu.m.	120	\$	1,100	\$		•	\$	132,000	<u> </u>
		Top Slab for Tank	cu.m.	90	\$	1,100	\$,	\$ -	\$	99,000	
		Mis. Metals	L.S.	1	\$	80,000	\$		\$ -	\$	80,000	<u> </u>
	3.4.5	Access Road and Parking Pad	L.S.	1	\$	20,000	\$	20,000	\$ -	\$	20,000	
	3.4.6	Superstructure + Architectural (Equipment Room, 4 m tall, steel frame with masonry infill)	sq.m.	150	\$	2,200	\$	330,000	\$ -	\$	330,000	I
3.5	Electric	, ,										\$105,000
		Motor Controls	Motors	3	\$	20,000	\$	60,000	\$ -	\$	60,000	
		Instruments and Control	L.S.	1	\$	40,000				\$	40,000	
	3.5.3	Integration	L.S.	1	\$	5,000	\$	5,000	\$ -	\$	5,000	
4.0 C		qualization Tank	•		•	· · · · · ·						\$ 4,177,000
4.1	Genera	al Requirements										\$836,000
	4.1.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and								\$	836,000	
4.0	Cita Ci	temporary work at 25% of project value)							Φ.			
4.2	Site Cl	vil, Access Road, and Landscaping	1				1		\$ -	_	1	\$322,000
	3.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	3,025	\$	5	\$		\$ -	\$	15,125	
		Tank Excavation and Backfilling	cu.m.	15,125	\$	15	\$, ,		\$	- ,	
		Inter-connecting Pipe Below Grade Pipework	li.m.	40	\$	2,000	\$	80,000	\$ -	\$	80,000	
4.3		s Mechanical								1 -		\$1,182,000
		Equalization Pumps	unit	2	\$	60,000		,	\$ 45,000		,	j
		Gates	unit	2	\$	50,000	\$		\$ 12,000		112,000	
		Connection to existing Odor System	li.m.	200	\$	1,000				\$	200,000	
		Pumps Pipes and Valves	L.S.	1	\$	180,000				\$	180,000	
	3.2.5	Mixing mixers	unit	8	\$	60,000	\$	480,000	\$ 45,000	\$	525,000	<u> </u>

Year

2017

2017

Title CVWPCC WWTF

Concept Design Cost Estimate for Option 3 - Phase I

Date

3-Aug-16

Description

Year Replace existing 12 mm mechanical screen with 6 mm screen 2017 Add grit removal tank c/w cyclones and classifiers units 2017 Decommissioning of existing primary sludge cyclones and classifiers 2017 and send the primary sludge directly to the sludge thickeners Injecting polymers prior cloth media filters (provision to be confirmed by pilot testing)
 Add cloth media filter 2017 2017 Construct offline equalization tank 2017 Repair of existing offshore pipe 2017

Additional Notes

Installation included unless otherwise stated

Items not included

Land procurement Costs

Contingency Allowances

Taxes

UV disinfection

	Item	Description .		Material	or Eq	uipment Co	st		Labor /	Total Line Item	Total Item Cost
item		Description	Unit	Quantity	Un	it Price (\$)	Aı	mount (\$)	Installation Costs (\$)	Cost (\$)	(\$)
4.4	Structu	ural									\$1,632,000
	3.4.1	Tank Walls	cu.m.	336	\$	1,500	\$	504,000	\$ -	\$ 504,000	
	3.4.2	Bottom Slab for Tank	cu.m.	613	\$	1,100	\$	673,750	\$ -	\$ 673,750	
	3.4.3	Top Slab for Tank	cu.m.	368	\$	1,100	\$	404,250	\$ -	\$ 404,250	
	3.4.4	Mis. Metals	L.S.	1	\$	30,000	\$	30,000	\$ -	\$ 30,000	
	3.4.5	Access Road and Parking Pad	L.S.	1	\$	20,000	\$	20,000	\$ -	\$ 20,000	
4.5	Electric	cal									\$205,000
	3.5.1	Motor Controls	Motors	8	\$	20,000	\$	160,000	\$ -	\$ 160,000	
	3.5.2	Instruments and control	L.S.	1	\$	40,000	\$	40,000	\$ -	\$ 40,000	
	3.5.3	Integration	L.S.	1	\$	5,000	\$	5,000	\$ -	\$ 5,000	
5.0 R	epair of	f existing outfall pipe									\$ 120,000
5.1		al Requirements									\$0
	4.1.1	Included in outfall sections costs								\$ -	
5.2	Repair	of existing outfall pipe									\$120,000
	4.2.1	Repair of existing outfall pipe	L.S.	1	\$	120,000	\$	120,000	\$ -	\$ 120,000	
		Total Capital Cost									\$11,063,000

Concept Design Cost Estimate for Option 3 - Phase 2

Date

3-Aug-16

Description

Year Construct one aeration tank and clarifier 2024 **Additional Notes**

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes
UV disinfection

		5		Material	or Ec	uipment Co	st		Labour /	То	otal Line Item	Total Item Cost
Item		Description	Unit	Quantity	Ur	nit Price (\$)	Am	ount (\$)	Installation Costs (\$)		Cost (\$)	(\$)
1.0 A	eration	Tank & Clarifier			'							\$ 4,720,000
1.1		al Requirements										\$944,00
		General requirement includes (overhead, indirect cost,										
	1.1.1	contractor profit, mobilization and demobilization and								\$	944,000	
		temporary work at 25% of project value)										
1.2	Site Ci	vil, Access Road, and Landscaping							\$ -			\$714,00
	1.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	2,725	\$	5	\$	13,625	\$ -	\$	13,625	
	1.2.2	Access Road and Parking Pad	L.S.	1	\$	100,000	\$	100,000	\$ -	\$	100,000	
		Inter-connecting Pipes Below Grade Pipework (from primary		252		•		·	•	<u> </u>		
	1.2.3	splitter to aeration tank)	li.m.	250	\$	1,500	\$	375,000	\$ -	\$	375,000	
	1.2.4	RAS and WAS piping	li.m.	50	\$	1,500	\$	75,000	\$ -	\$	75,000	
		Air piping	li.m.	100	\$	1,500	\$	150,000		\$	150,000	
1.3		ss Mechanical										\$1,670,00
	1.3.1	Fine bubble diffusers and air pipes	L.S.	1	\$	280,000	\$	280,000	\$ 180,000	\$	460,000	
	1.3.2	Mixer	unit	1	\$	60,000	\$	60,000	\$ 12,000	\$	72,000	
	1.3.3	Clarifier Mechanism	L.S.	1	\$	506,000	\$	506,000	\$ 180,000	\$	686,000	
	1.3.4	RAS/WAS pumping	unit	4	\$	60,000	\$	240,000	\$ 12,000	\$	252,000	
	1.3.5	RAS/WAS Valves and Pipes	L.S.	1	\$	200,000	\$	200,000	\$ -	\$	200,000	
1.4	Structi		•			,					·	\$1,161,00
	1.4.1	Aeration Tank Walls	cu.m.	313	\$	1,500	\$	468,750	\$ -	\$	468,750	
	1.4.2	Bottom Slab for Aeration Tank	cu.m.	260	\$	1,100	\$	286,000	\$ -	\$	286,000	
	1.4.3	Access stairs	cu.m.	26	\$	1,500	\$	39,000		\$	39,000	
	1.4.4	Handrail (Install Inc.)	li.m	170	\$	150	\$	25,500	\$ -	\$	25,500	
	1.4.5	Clarifier Walls	cu.m.	157	\$	1,500	\$	235,242	\$ -	\$	235,242	
		Bottom Slab for Clarifier Tank	cu.m.	30	\$	1,100	\$	33,175		\$	33,175	
		Access Stairs	cu.m.	8	\$	1,500	\$	11,310		\$	11,310	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$	50,000		\$	50,000	
	1.4.9	Handrail (Install Inc.)	li.m	75	\$	150	\$	11,310	\$ -	\$	11,310	
1.5	Plumb		•		-		-					\$50,00
		Plumbing	L.S.	1	\$	50,000	\$	50,000	\$ -	\$	50,000	
1.6	Electri											\$182,00
		Motor Controls	Motors	4	\$	10,000		40,000		\$	40,000	
		Instruments and Controls	L.S.	1	\$	130,000	\$	130,000		\$	130,000	
	1.6.3	Integration	L.S.	1	\$	12,000	\$	12,000	\$ -	\$	12,000	
		Total Capital Cost										\$4,721,00

Concept Design Cost Estimate for Option 3 - Phase 3

Date

3-Aug-16

Description Replace all outfall sections (onshore/offshore)

2033 Construct two primary clarifiers and process building Upgrade cloth media filter 2034 Upgrade effluent pumps 2043 Add mechanical screens to new process building

2045 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056 Install new centrifuge 2060

 Construct one aeration tank and clarifier 2063 **Additional Notes**

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes UV disinfection

Capital Cost Estimate

				Material	or Ed	quipment Co	st		١.	Labor /	То	tal Line Item	Tot	al Item Cost
Item		Description	Unit	Quantity	Ur	nit Price (\$)	Α	mount (\$)		nstallation Costs (\$)		Cost (\$)		(\$)
I.0 R	eplace	Outfall Sections (Onshore/Offshore) - Year (2031)	'		-								\$	14,109,000
1.1		al Requirements												\$
		Included in outfall sections costs									\$	-		
1.2	Civil								\$	-				\$13,949,00
	1.2.1	900 mm Tie-In and temporary works	L.S.	1	\$	40,000	_	40,000	\$	-	\$	40,000		
		Onshore Section (2827.0 m Length)	L.S.	1	\$	7,633,000	\$	7,633,000		-	\$	7,633,000		
		Offshore section (2825.0 m Length)	L.S.	1	\$	6,215,000		6,215,000		-	\$	6,215,000		
		Diffuser section (175.0 m Length)	L.S.	11	\$	61,000	\$	61,000	\$	-	\$	61,000		
1.3		nical and Electrical	1								_			\$160,00
		Add fourth pump	L.S.	1	\$	150,000		150,000		-	\$	150,000		
		Integration	L.S.	11	\$	10,000	\$	10,000	\$	-	\$	10,000		
		Clarifiers + Process Building - Year (2033)											\$	7,650,000
2.1		al Requirements	1		_				1					\$1,530,00
		General requirement includes (overhead, indirect cost,									_	4 500 000		
		contractor profit, mobilization and demobilization and									\$	1,530,000		
		temporary work at 25% of project value)							_					<u> </u>
2.2		vil, Access Road, and Landscaping							\$	-				\$219,00
		Site Clearing/ Stripping and Stockpile (Area of building and tank plus 10m, perimeter)	sq.m.	3,687	\$	5	\$	18,435	\$	-	\$	18,435		
	222	Access Road and Parking Pad	L.S.	1	\$	200,000	\$	200,000	\$	_	\$	200,000		
2.3		s Mechanical	2.0.	•	ŢΨ	200,000	Ψ	200,000	Ψ		Ψ	200,000		\$2,568,00
		Primary Clarifier Mechanism	L.S.	2	\$	360.000	\$	720,000	\$	180.000	\$	900.000		+ =,000,00
		Air Blowers	L.S.	5	\$	150,000	\$	750,000	\$	180,000	\$	930,000		
		WAS pumping	unit	2	\$	60,000	\$	120,000		12,000	\$	132,000		
		WAS Valves and Pipes	L.S.	1	\$	150,000		150,000		-	\$	150,000		
	2.3.5	Air Valves and Pipes	L.S.	1	\$	250,000		250,000	\$	-	\$	250,000		
		Sluice Gates	unit	4	\$	50,000	\$	200,000		6,000	\$	206,000		
2.4	Structu							·		·				\$2,402,00
	2.4.1	Primary Tank Walls	cu.m.	150	\$	1,500	\$	225,000		_	\$	225,000		
	2.4.2	Bottom Slab for Primary Tank	cu.m.	160	\$	1,100	\$	176,000	\$	_	\$	176,000		
		Access stairs	cu.m.	16	\$	1,500	\$	24,000		-	\$	24,000		
		Process Building	cu.m.	250	\$	1,500	\$	375,000			\$	375,000		
		Bottom Slab for Process Building	cu.m.	216	\$	1,100	\$	237,600		-	\$	237,600		
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	150,000	\$	150,000		-	\$	150,000		
		Handrail (Install Inc.)	li.m	170	\$	150	\$	25,500	\$	-	\$	25,500		
	2.4.8	Superstructure + Architectural (Process Building, 6 m tall, steel frame with masonry infill)	sq.m.	540	\$	2,200	\$	1,188,000	\$	-	\$	1,188,000		
2.5		ing & HVAC												\$800,00
		Plumbing	L.S.	1	\$	300,000	\$	300,000	\$	-	\$	300,000		, ,
	2.5.2	HVAC	L.S.	<u>·</u> 1	\$	500,000	\$	500,000		-	\$			
2.6	Electric		-			-,		-,				-,		\$132,00
		Motor Controls	Motors	4	\$	10,000	\$	40,000	\$	-	\$	40,000		,
		Instruments and Controls	L.S.	1	\$	80,000	\$	80,000		-	\$	80,000		
		Integration	L.S.	1	\$	12,000	\$	12,000		-	\$	12,000		

Year

2031

Concept Design Cost Estimate for Option 3 - Phase 3

Date

3-Aug-16

Description Year Replace all outfall sections (onshore/offshore) 2031 Construct two primary clarifiers and process building 2033

 Upgrade cloth media filter 2034 Upgrade effluent pumps 2043 Add mechanical screens to new process building 2045 Add grit removal tank c/w cyclones and classifiers units 2045

 Construct new thickener 2056 Install new centrifuge 2060

 Construct one aeration tank and clarifier 2063 **Additional Notes**

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes

UV disinfection

		Beautifica		Material	or E	quipment Co	st			Labor /	То	tal Line Item	Total	Item Cost
Item		Description	Unit	Quantity	U	nit Price (\$)	1	Amount (\$)		nstallation Costs (\$)		Cost (\$)		(\$)
3.0 M	edia Clo	oth Filter (2034)											\$	1,759,00
3.1	Genera	al Requirements												\$352,00
		General requirement includes (overhead, indirect cost,												
	3.1	contractor profit, mobilization and demobilization and									\$	352,000		
		temporary work at 25% of project value)												
3.2		ss Mechanical												\$1,322,00
		Modification to Polymer Injection System	unit	1	\$	30,000		30,000	_	12,000		42,000		
		Cloth media filter equipment	unit	1	\$	1,050,000	_		_	180,000		1,230,000		
		Pipes and Valves	L.S.	1	\$	50,000	\$	50,000	\$	-	\$	50,000		
3.3	Electric													\$85,00
		Motor Controls	Motors	2	\$	20,000				-	\$	40,000		
		Instruments and Control	L.S.	1	\$	40,000	_		_	-	\$	40,000		
	3.3.3	Integration	L.S.	1	\$	5,000	\$	5,000	\$	-	\$	5,000		
		Pumps - Year (2043)											\$	1,780,00
4.1		al Requirements												
	5.1.1	Included in effluent pumps item costs									\$	-		
4.2		vil, Access Road, and Landscaping				,						,		\$50,0
		Interconnecting pipes within CVWPCC	L.S.	1	\$	50,000	\$	50,000	\$	-	\$	50,000		
4.3		s Mechanical												\$1,200,0
		Replace existing pumps	L.S.	1	\$	600,000				-	\$	600,000		
		Valves and pipes (within the vault)	L.S.	1	\$	600,000	\$	600,000	\$	-	\$	600,000		
4.4	Structu					,						,		\$80,00
		New outfall chamber	L.S.	1	\$	80,000	\$	80,000	\$	-	\$	80,000		
4.5	Electric													\$450,00
		Electrical	L.S.	11	\$	370,000	_	370,000	_	-	\$	370,000		
		Instruments and control	L.S.	1	\$	80,000	\$	80,000	\$	-	\$	80,000		
		cal Screen - Year (2045)											\$	892,00
5.1		al Requirements				-						-		\$179,0
		General requirement includes (overhead, indirect cost,												
		contractor profit, mobilization and demobilization and									\$	179,000		
		temporary work at 25% of project value)												
5.2		ss Mechanical												\$648,00
		Mechanical Screen c/w Washer and Compactor	L.S.	2	\$	300,000	\$	600,000	\$	48,000	\$	648,000		4
5.3	Electric		T		-		_	10.000	•			10.000		\$65,00
		Motor Controls	Motors	2	\$	20,000				-	\$	40,000		
		Instruments and control	L.S.	1	\$	20,000				-	\$	20,000		
0 0		Integration	L.S.	1	\$	5,000	\$	5,000	\$		\$	5,000	^	1.040.00
		oval - Year (2045)											\$	1,013,00
6.1		al Requirements	1			1		1				1		\$203,0
		General requirement includes (overhead, indirect cost,										202 222		
		contractor profit, mobilization and demobilization and									\$	203,000		
		temporary work at 25% of project value)	1 1				<u> </u>		Φ.		<u> </u>			6440.0
6.2	Site Ci	vil, Access Road, and Landscaping	1			1			\$	-	1	1		\$119,00
	6.2.1	Site Clearing/ Stripping and Stockpile (Area of chamber plus	sq.m.	225	\$	5	\$	1,125	\$	-	\$	1,125		
	600	10m, perimeter)		1 170	•	4.5	,					17.550		
		Chamber Excavation and Backfilling	cu.m.	1,170	\$	15	\$	17,550		-	\$	17,550		
	6.2.3	Inter-connecting Pipe Below Grade Pipework	li.m.	50	\$	2,000	- \$	100,000	\$	-	\$	100,000		

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Concept Design Cost Estimate for Option 3 - Phase 3

Date

3-Aug-16

 Description
 Year

 ● Replace all outfall sections (onshore/offshore)
 2031

Construct two primary clarifiers and process building
 Upgrade cloth media filter
 Upgrade effluent pumps
 Add mechanical screens to new process building
 2034
 2043

Add grit removal tank c/w cyclones and classifiers units
 Construct new thickener
 Install new centrifuge

• Construct one aeration tank and clarifier 2063

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes
UV disinfection

No.		Description		Material	or Eq	uipment Co	st	Labor /	Total Line Item	Total Item Cost
Item		Description	Unit	Quantity	Un	it Price (\$)	Amount (\$)	Installation Costs (\$)	Cost (\$)	(\$)
6.3	Proces	ss Mechanical						•		\$480,000
	6.3.1	Grit Removal Equipment	L.S.	1	\$	300,000			\$ 348,000	
		Sluice Gates	unit	2	\$					
	6.3.3	Connection to existing Odor System	L.S.	1	\$	10,000			\$ 10,000	
		Weirs for splitter box	L.S.	1	\$	10,000	\$ 10,000	\$ -	\$ 10,000	
6.4	Structu									\$146,000
		Concentrator and Channels Walls	cu.m.	44	\$	1,500	\$ 66,007		\$ 66,007	
		Bottom Slab for Concentrator and Channel	cu.m.	22	\$	1,100	\$ 24,241		\$ 24,241	
		Top Slab for Concentrator	cu.m.	19	\$	1,500	\$ 27,778		\$ 27,778	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000			\$ 20,000	
		Handrail (Install Inc.)	li.m	16	\$	150	\$ 2,356		\$ 2,356	
		Access Road and Parking Pad	L.S.	1	\$	5,000	\$ 5,000	\$ -	\$ 5,000	
6.5	Electri		,							\$65,000
		Motor Controls	Motors	2	\$	20,000			\$ 40,000	
		Instruments and control	L.S.	1	\$	20,000			\$ 20,000	
	6.5.3	Integration	L.S.	1	\$	5,000	\$ 5,000	\$ -	\$ 5,000	
		er - Year (2056)								\$ 1,072,000
7.1	Genera	al Requirements								\$215,000
		General requirement includes (overhead, indirect cost,								
		contractor profit, mobilization and demobilization and							\$ 215,000	
		temporary work at 25% of project value)								
7.2	Site Ci	vil, Access Road, and Landscaping						\$ -		\$144,000
	7.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	800	\$	5	\$ 4,000	\$ -	\$ 4,000	
		Access Road and Parking Pad	L.S.	1	\$	40,000	\$ 40,000	\$ -	\$ 40,000	
		Inter-connecting Pipes Below Grade Pipework	L.S.	1	\$	100,000	\$ 100,000	\$ -	\$ 100,000	
7.3		ss Mechanical								\$480,000
		Thickener Mechanism	L.S.	1	\$	250,000		\$ 180,000		
	7.3.2	Connection to existing Odor System	L.S.	1	\$	50,000	\$ 50,000		\$ 50,000	
7.4	Structu									\$198,000
		Thickener Tank Walls	cu.m.	32	\$	1,500			\$ 48,000	
		Bottom Slab for Thickener Tank	cu.m.	63	\$	1,100	\$ 69,300		\$ 69,300	
		Thickener cover	L.S.	11	\$	30,000			\$ 30,000	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$ 50,000	\$ -	\$ 50,000	
7.5	Electri									\$35,000
		Motor Controls	Motors	1	\$	10,000			\$ 10,000	
		Instruments and Controls	L.S.	11	\$	20,000			\$ 20,000	
		Integration	L.S.	1	\$	5,000	\$ 5,000	\$ -	\$ 5,000	
		ge - Year (2060)								\$ 1,190,000
8.1	Genera	al Requirements								\$238,000
		General requirement includes (overhead, indirect cost,								
	8.1.1	contractor profit, mobilization and demobilization and							\$ 238,000	
		temporary work at 25% of project value)						<u> </u>		
8.2	Site Ci	vil, Access Road, and Landscaping						\$ -		\$57,000
	8.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	1,225	\$	5	\$ 6,125	\$ -	\$ 6,125	
	8.2.2	Inter-connecting Pipes Below Grade Pipework	L.S.	1	\$	50,000	\$ 50,000	\$ -	\$ 50,000	

Concept Design Cost Estimate for Option 3 - Phase 3

Date

3-Aug-16

Description Year Replace all outfall sections (onshore/offshore) 2031

2033 Construct two primary clarifiers and process building Upgrade cloth media filter 2034 Upgrade effluent pumps 2043 Add mechanical screens to new process building 2045

 Add grit removal tank c/w cyclones and classifiers units 2045 Construct new thickener 2056 Install new centrifuge 2060 2063

Construct one aeration tank and clarifier

Additional Notes

Installation included unless otherwise stated

Items not included Land procurement Costs Contingency Allowances

Taxes UV disinfection

				Material	or Eq	uipment Co	st		Labor / Installation		To	otal Line Item	Total Item Cost
Item		Description	Unit	Quantity	Un	nit Price (\$)	Α	mount (\$)		Installation Costs (\$)		Cost (\$)	(\$)
8.3	Proces	s Mechanical											\$530,000
	8.3.1	Centrifuge	L.S.	1	\$	350,000	\$	350,000	\$	180,000	\$	530,000	
8.4	Structu												\$330,000
		Centrifuge base based on extending existing structure	cu.m.	60	\$	1,500	\$	90,000	\$	-	\$	90,000	
	8.4.2	Superstructure + Architectural (Chemical Room, 6 m tall, steel	sq.m.	100	\$	2,200	\$	220,000	¢	_	\$	220,000	
		frame with masonry infill)											
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	20,000	\$	20,000	\$	-	\$	20,000	
8.5	Electric												\$35,000
		Motor Controls	Motors	1	\$	10,000		10,000			\$		
		Instruments and Controls	L.S.	1	\$	20,000		20,000			\$		
		Integration	L.S.	1	\$	5,000	\$	5,000	\$	-	\$	5,000	
		on Tank and Clarifier - Year (2063)											\$ 4,252,000
9.1		al Requirements					,						\$851,000
		General requirement includes (overhead, indirect cost,											
		contractor profit, mobilization and demobilization and									\$	851,000	
		temporary work at 25% of project value)											
9.2		vil, Access Road, and Landscaping					,		\$	-			\$339,000
	9.2.1	Site Clearing/ Stripping and Stockpile (Area of tank plus 10m, perimeter)	sq.m.	2,725	\$	5	\$	13,625	\$	-	\$	13,625	
	9.2.2	Access Road and Parking Pad	L.S.	1	\$	100,000	\$	100,000	\$	-	\$	100,000	
	9.2.3	RAS and WAS piping	L.S.	1	\$	75,000	\$	75,000	\$	-	\$	75,000	
	9.2.4	Air piping	li.m.	100	\$	1,500	\$	150,000	\$	-	\$	150,000	
9.3		s Mechanical					•					•	\$1,670,000
	9.3.1	Fine bubble diffusers and air pipes	L.S.	1	\$	280,000	\$	280,000	\$	180,000	\$		
	9.3.2	Mixer	unit	1	\$	60,000	\$	60,000	\$	12,000	\$	72,000	
		Clarifier Mechanism	L.S.	1	\$	506,000		506,000				686,000	
	9.3.4	RAS/WAS pumping	unit	4	\$	60,000		240,000		12,000	\$		
	9.3.5	RAS/WAS Valves and Pipes	L.S.	1	\$	200,000	\$	200,000	\$	-	\$		
9.4	Structu	ıral											\$1,161,000
	9.4.1	Aeration Tank Walls	cu.m.	313	\$	1,500	\$	468,750	\$	-	\$		
	9.4.2	Bottom Slab for Aeration Tank	cu.m.	260	\$	1,100	\$	286,000	\$	-	\$	286,000	
	9.4.3	Access stairs	cu.m.	26	\$	1,500		39,000			\$		
	9.4.4	Handrail (Install Inc.)	li.m	170	\$	150		25,500			\$		
		Clarifier Walls	cu.m.	157	\$	1,500	\$	235,242	\$	-	\$		
		Bottom Slab for Clarifier Tank	cu.m.	30	\$	1,100	\$	33,175	\$	-	\$	33,175	
		Access Stairs	cu.m.	8	\$	1,500	\$	11,310			\$	11,310	
		Concrete Walkways / Access Ramp / Road	L.S.	1	\$	50,000	\$	50,000	\$	-	\$		
		Handrail (Install Inc.)	li.m	75	\$	150	\$	11,310	\$	-	\$	11,310	
9.5	Plumbi	ing											\$50,000
	9.5.1	Plumbing	L.S.	1	\$	50,000	\$	50,000	\$	-	\$	50,000	
9.6	Electric	cal					•						\$182,000
		Motor Controls	Motors	4	\$	10,000		40,000			\$		
	9.6.2	Instruments and Controls	L.S.	1	\$	130,000		130,000	\$	-	\$		
		Integration	L.S.	1	\$	12,000		12,000	\$	-	\$		
		Total Capital Cost											\$33,718,000

Project Name / Number

31548 CVWPCC WWTF

Title

Concept Design Cost Estimate

Date

26-Jun-16

Description

	Phase 1 - 2017 Construction		
Item	Description	Option 3	Option 9
1.0	Mechanical Screen	\$ 452,000	\$ 452,000
1.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 91,000	\$ 91,000
1.2	Mechanical Screen c/w Washer and Compactor	\$ 260,000	\$ 260,000
1.3	Sluice Gates	\$ 56,000	\$ 56,000
1.4	Electrical	\$ 45,000	\$ 45,000
2.0	Grit Removal	\$ 1,025,000	\$ 1,025,000
2.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 205,000	\$ 205,000
2.2	Site Civil, Access Road, and Landscaping	\$ 119,000	\$ 119,000
2.3	Grit Removal Equipment	\$ 348,000	\$ 348,000
2.4	Sluice Gates	\$ 112,000	\$ 112,000
2.5	Connection to existing Odor System	\$ 10,000	\$ 10,000
2.6	Weirs for splitter box	\$ 10,000	\$ 10,000
2.7	Structural	\$ 146,000	\$ 146,000
2.8	Electrical	\$ 65,000	\$ 65,000
2.9	Decommissioning	\$ 10,000	\$ 10,000
3.0	Offline Equalization Tank	\$ 4,177,000	\$ 4,177,000
3.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 836,000	\$ 836,000
3.2	Site Civil, Access Road, and Landscaping	\$ 322,000	\$ 322,000
3.3	Equalization Pumps	\$ 165,000	\$ 165,000
3.4	Gates	\$ 112,000	\$ 112,000
3.5	Connection to existing Odor System	\$ 200,000	\$ 200,000
3.6	Pumps Pipes and Valves	\$ 180,000	\$ 180,000
3.7	Mixing mixers	\$ 525,000	\$ 525,000
3.8	Structural	\$ 1,632,000	\$ 1,632,000
3.9	Electrical	\$ 205,000	\$ 205,000

Project Name / Number

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Title

Concept Design Cost Estimate

Date

26-Jun-16

Description

	Phase 1 - 2017 Construction		
Item	Description	Option 3	Option 9
4.0	Chemical Treatment	\$ -	\$ -
4.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)		
4.2	Site Civil, Access Road, and Landscaping		
4.3	Soda Ash Super Bag System		
4.4	Polymer Injection System		
4.5	Pipes and Valves		
4.6	Structural		
4.7	HVAC / Plumbing System		
4.8	Electrical		
5.0	Aeration Tank & Clarifier	\$ -	\$ -
5.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)		
5.2	Site Civil, Access Road, and Landscaping		
5.3	Fine bubble diffusers and air pipes		
5.4	Mixer		
5.5	Clarifier Mechanism		
5.6	RAS/WAS pumping		
5.7	RAS/WAS Valves and Pipes		
5.8	Structural		
5.9	Plumbing		
5.10	Electrical		

Project Name / Number

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Title

Concept Design Cost Estimate

Date

26-Jun-16

Description

Phase 1 - 2017 Construction										
Item	Description		Option 3		Option 9					
6.0	Repair of existing outfall pipe	\$	120,000	\$	120,000					
6.1	General requirments included in the repairs costs	\$	-	\$	-					
6.2	Repair of existing outfall pipe	\$	120,000	\$	120,000					
7.0	Media Cloth Filter	\$	5,289,000	\$	-					
7.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$	1,058,000	\$	-					
7.2	Site Civil, Access Road, and Landscaping	\$	208,000	\$	-					
7.3	Polymer Injection System	\$	112,000	\$	-					
7.4	Cloth media filter equipment	\$	1,755,000	\$	-					
7.5	Sluice Gates	\$	612,000	\$	-					
7.6	Pipes and Valves	\$	250,000	\$	-					
7.7	Structural	\$	1,189,000	\$	-					
7.8	Electrical	\$	105,000	\$	-					
8.0	Fourth Clarifer	\$	-	\$	2,168,000					
8.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)			\$	434,000					
8.2	Site Civil, Access Road, and Landscaping			\$	304,000					
8.3	Clarifier Mechanism			\$	686,000					
8.4	Polymer injection system (provision)			\$	112,000					
8.5	RAS/WAS Valves and Pipes			\$	200,000					
8.6	Structural			\$	392,000					
8.7	Electrical			\$	40,000					

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Item	Description	Option 3	Option 9
8.0	Effluent Reuse Package	\$ -	\$ 863,000
8.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)		\$ 173,000
8.2	Pipes for cloth media filter to the headwork		\$ 50,000
8.3	Effluent filteration package		\$ 330,000
8.4	Effluent reuse valves and pipes		\$ 120,000
8.6	Increase in the UV building to accommodate cloth media filter		\$ 120,000
8.7	Electrical		\$ 70,000
9.0	Upgrade Effluent Pumps	\$ -	\$ -
9.1	General requirments included in effluent pumps item costs		
9.2	Upgrade of existing effluent pumps and new outfall chamber	\$ -	\$ -
	Capital Costs	\$ 11,063,000	\$ 8,805,000
	Engineering and Contingencies (40%)	\$ 4,426,000	\$ 3,522,000
	Total Capital Costs	\$ 15,489,000	\$ 12,327,000

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Title

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	Phase 2 - 2024 Construction		
ltem	Description	Option 3	Option 9
1.0	Aeration Tank & Clarifier	\$ 4,721,000	\$ 4,721,000
1.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 944,000	\$ 944,000
1.2	Site Civil, Access Road, and Landscaping	\$ 714,000	\$ 714,000
1.3	Fine bubble diffusers and air pipes	\$ 460,000	\$ 460,000
1.4	Mixer	\$ 72,000	\$ 72,000
1.5	Clarifier Mechanism	\$ 686,000	\$ 686,000
1.6	RAS/WAS pumping	\$ 252,000	\$ 252,000
1.7	RAS/WAS Valves and Pipes	\$ 200,000	\$ 200,000
1.8	Structural	\$ 1,161,000	\$ 1,161,000
1.9	Plumbing	\$ 50,000	\$ 50,000
1.10	Electrical	\$ 182,000	\$ 182,000
	Capital Costs	\$ 4,721,000.00	\$ 4,721,000.00
	Engineering and Contingencies (40%)	\$ 1,889,000	\$ 1,889,000
	Total Capital Costs	\$ 6,610,000	\$ 6,610,000

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Title

Concept Design Cost Estimate

Date

26-Jun-16

	Phase 3 - Varies		
Item	Description	Option 3	Option 3
1.0	Replace Outfall Sections (Onshore/Offshore) - Year (2031)	\$ 13,949,000	\$ 13,949,000
1.1	General requirements (included in the Outfall items costs)	\$ -	\$ -
1.2	900 mm Tie-In and temporary works	\$ 40,000	\$ 40,000
1.3	Onshore Section (2827.0 m Length)	\$ 7,633,000	\$ 7,633,000
1.4	Offshore section (2825.0 m Length)	\$ 6,215,000	\$ 6,215,000
1.5	Diffuser section (175.0 m Length)	\$ 61,000	\$ 61,000
1.6	Add fourth pump	\$ -	\$ -
	Capital Costs	\$ 13,949,000.00	\$ 13,949,000.00
	Engineering and Contingencies (40%)	\$ 5,580,000	\$ 5,580,000
	Total Capital Costs	\$ 19,529,000	\$ 19,529,000
2.0	Primary Clarifiers + Process Building - Year (2033)	\$ 7,651,000	\$ 7,651,000
2.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 1,530,000	\$ 1,530,000
2.2	Site Civil, Access Road, and Landscaping	\$ 219,000	\$ 219,000
2.3	Primary Clarifier Mechanism	\$ 900,000	\$ 900,000
2.4	Air Blowers	\$ 930,000	\$ 930,000
2.5	WAS pumping	\$ 132,000	\$ 132,000
2.6	WAS Valves and Pipes	\$ 150,000	\$ 150,000
2.7	Air Valves and Pipes	\$ 250,000	\$ 250,000
2.8	Sluice Gates	\$ 206,000	\$ 206,000
2.9	Structural	\$ 2,402,000	\$ 2,402,000
2.10	Plumbing & HVAC	\$ 800,000	\$ 800,000
2.12	Electrical	\$ 132,000	\$ 132,000
	Capital Costs	\$ 7,651,000.00	\$ 7,651,000.00
	Engineering and Contingencies (40%)	\$ 3,061,000	\$ 3,061,000
	Total Capital Costs	\$ 10,712,000	\$ 10,712,000

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Title

Concept Design Cost Estimate

Date

26-Jun-16

Description	Phase 3 - Varies		
Item	Description	Option 3	Option 3
4.0	Upgrade Media Cloth Filter - Year (2034)	\$ 1,759,000	\$ -
4.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 352,000	\$ -
4.2	Modification to Polymer Injection System	\$ 42,000	\$ -
4.3	Cloth media filter equipment	\$ 1,230,000	\$ -
4.4	Pipes and Valves	\$ 50,000	\$ -
4.5	Electrical	\$ 85,000	\$ -
	Capital Costs	\$ 1,759,000.00	\$ -
	Engineering and Contingencies (40%)	\$ 704,000	\$ -
	Total Capital Costs	\$ 2,463,000	\$ -
5.0	Effluent Pumps - Year (2043)	\$ 1,780,000	\$ 1,780,000
5.1	General requirements (included in the Effluent Pumps items costs)	\$ -	\$ -
5.2	Site Civil, Access Road, and Landscaping	\$ 50,000	\$ 50,000
5.3	Replace existing pumps	\$ 600,000	\$ 600,000
5.4	Valves and pipes (within the vault)	\$ 600,000	\$ 600,000
5.5	Structural	\$ 80,000	\$ 80,000
5.6	Electrical	\$ 450,000	\$ 450,000
	Capital Costs	\$ 1,780,000.00	\$ 1,780,000.00
	Engineering and Contingencies (40%)	\$ 712,000	\$ 712,000
	Total Capital Costs	\$ 2,492,000	\$ 2,492,000
6.0	Mechanical Screen - Year (2045)	\$ 892,000	\$ 892,000
6.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 179,000	\$ 179,000
6.2	Mechanical Screen c/w Washer and Compactor	\$ 648,000	\$ 648,000
6.3	Electrical	\$ 65,000	\$ 65,000

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Title

Concept Design Cost Estimate

Date

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	Phase 3 - Varies		
Item	Description	Option 3	Option 3
7.0	Grit Removal - Year (2045)	\$ 1,013,000	\$ 1,013,000
7.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 203,000	\$ 203,000
7.2	Site Civil, Access Road, and Landscaping	\$ 119,000	\$ 119,000
7.3	Grit Removal Equipment	\$ 348,000	\$ 348,000
7.4	Sluice Gates	\$ 112,000	\$ 112,000
7.5	Connection to existing Odor System	\$ 10,000	\$ 10,000
7.6	Weirs for splitter box	\$ 10,000	\$ 10,000
7.7	Structural	\$ 146,000	\$ 146,000
7.8	Electrical	\$ 65,000	\$ 65,000
8.0	Expand Chemical Treatment - Year (2045)		
8.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)		
8.2	Civil		
8.3	Add soda ash injection pump		
8.4	Add polymer Injection pump		
8.5	Pipes and Valves		
8.6	Electrical		
	Capital Costs	\$ 1,905,000.00	\$ 1,905,000.00
	Engineering and Contingencies (40%)	\$ 762,000	\$ 762,000
	Total Capital Costs	\$ 2,667,000	\$ 2,667,000

31548 CVWPCC WWTF

Title

Concept Design Cost Estimate

Date

26-Jun-16

	Phase 3 - Varies		
Item	Description	Option 3	Option 3
9.0	Thickener - Year (2056)	\$ 1,072,000	\$ 1,072,000
9.1	General requirement includes (overhead, indirect cost, contractor profit,	\$ 215,000	\$ 215,000
	mobilization and demobilization and temporary work at 25% of project value)		
9.2	Site Civil, Access Road, and Landscaping	\$ 144,000	\$ 144,000
9.3	Thickener Mechanism	\$ 430,000	\$ 430,000
9.4	Connection to existing Odor System	\$ 50,000	\$ 50,000
9.5	Structural	\$ 198,000	\$ 198,000
9.6	Electrical	\$ 35,000	\$ 35,000
	Capital Costs	\$ 1,072,000.00	\$ 1,072,000.00
	Engineering and Contingencies (40%)	\$ 429,000	\$ 429,000
	Total Capital Costs	\$ 1,501,000	\$ 1,501,000
10.0	Centrifuge - Year (2060)	\$ 1,190,000	\$ 1,190,000
10.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 238,000	\$ 238,000
10.2	Site Civil, Access Road, and Landscaping	\$ 57,000	\$ 57,000
10.3	Centrifuge	\$ 530,000	\$ 530,000
10.4	Structural	\$ 330,000	\$ 330,000
10.5	Electrical	\$ 35,000	\$ 35,000
	Capital Costs	\$ 1,190,000.00	\$ 1,190,000.00
	Engineering and Contingencies (40%)	\$ 476,000	\$ 476,000
	Total Capital Costs	\$ 1,666,000	\$ 1,666,000

31548 CVWPCC WWTF

Title

Concept Design Cost Estimate

Date

26-Jun-16

Item	Description	Option 3	Option 3
11.0	Aertation Tank and Clarifier - Year (2063)	\$ 4,253,000	\$ 4,253,000
11.1	General requirement includes (overhead, indirect cost, contractor profit, mobilization and demobilization and temporary work at 25% of project value)	\$ 851,000	\$ 851,000
11.2	Site Civil, Access Road, and Landscaping	\$ 339,000	\$ 339,000
11.3	Fine bubble diffusers and air pipes	\$ 460,000	\$ 460,000
11.4	Mixer	\$ 72,000	\$ 72,000
11.5	Clarifier Mechanism	\$ 686,000	\$ 686,000
11.6	RAS/WAS pumping	\$ 252,000	\$ 252,000
11.7	RAS/WAS Valves and Pipes	\$ 200,000	\$ 200,000
11.8	Structural	\$ 1,161,000	\$ 1,161,000
11.9	Plumbing	\$ 50,000	\$ 50,000
11.10	Electrical	\$ 182,000	\$ 182,000
	Capital Costs	\$ 4,253,000.00	\$ 4,253,000.00
	Engineering and Contingencies (40%)	\$ 1,702,000	\$ 1,702,000
	Total Capital Costs	\$ 5,955,000	\$ 5,955,000

Equalization Tank Operating Hours	hrs/year	500
Effluent Pumps Operating Hours	hrs/year	80
kWh cost	\$/kWh	0.1
Yearly Heating & Ventilation Cost	\$/m ²	13
Repair and Annual Replacement Cost		2%
Soda Ash Cost	\$/kg	1

Rated power/unit	g & Ventilation Filter Building
Flow/unit	
Head	
Efficiency Power consumed per unit Building area Operation Annual Power Annual Power Cost/Unit \$ Design average flow (2043) Alkalinity gain Swhere Swhe	
Power consumed per unit RWh A.1 18.2 1.2 5.8 2.5 105.7 5.0 100 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150 150	
Building area m² hrs/year 500 500 8760 730 8760 80 2000 8760 8760 8760 Annual Power Cost/Unit \$ \$ 207 908 1089 424 2178 846 995 1300 1950	
Operation	
Annual Power	
Annual Power Cost/Unit \$ \$ 207 908 1089 424 2178 846 995 1300 1950 Design average flow (2043) Estimated required alkalinity Mg/L as CaCO ₃ mg/L per mg/L of Na ₂ CO ₃ Mg/L as CaCO ₃ mg/L per mg/L of Na ₂ CO ₃	8760
Design average flow (2043) Estimated required alkalinity mg/L as CaCO ₃ Alkalinity gain MLD mg/L as CaCO ₃ 0.9	
Estimated required alkalinity mg/L as CaCO ₃ 50. Alkalinity gain mg/L per mg/L of Na ₂ CO ₃ 0.5	
Alkalinity gain mg/L per mg/L of Na ₂ CO ₃ 0.9	22
Alkalinity gain $\int_{0.5}^{0.5} \int_{0.5}^{0.5} d \cdot Na_2 CO_3^2 = 0.5$	50.0
Sodium hypochlorite system	0.9
Journal Hypothionic System	
Concentration 100	100%
Dose	55.6
Consumption liter/year 446,1	446,147
	446,147
Mechanical capital cost \$ 525,000 165,000 50,000 800,000 600,000	
Number of units 6 2 3 2 1 3 1	
Repairs and annual filter replacement	
cost (2% of mechanical cost)/unit \$ 1,750 1,650 7,900 500 16,000 4,000 2,500	

Cloth media disk filter cost includes \$6510/filter/year unit, calculated based on replacing the filter media every 20 years

Part										Option 3 C	perating Co	st								
2018 159 8 8 1658 2 1 908 3 2 2,178 2 1 424 1950 42,000 49,119		ج	Equ	ualization Mi	ixing	Equalia	zation Tank	c pumps	(Cloth Media Fi	lter	Ва	ackwash pum	ps	Efflo	uent pum	ps	HVAC	Rej anr rep cos	Tog
2019 16.2 6	Year	verage Flow	Total units			Total units		Yearly Cost	Total units			Total units		Yearly Cost	Total units		Yearly Cost		pairs and nual blacement st	tal Cost
2020 16.5 8	2018	15.9	8	8	1,658	2	1	908	3	2	2,178	2	1	424				1950	42,000	49,119
2021 16.8 8					,						, -		1						,	-, -
2022 17.1 8													1							
2023 17.3 8 8 1,668 2 1 908 3 2 2,178 2 1 424 1950 42,000 49,119													1							
2024 17.5 8 8 1658 2 1 998 3 2 2.178 2 1 424 1990 42.000 49.119													1							
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2026 18.0 8													1							
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2028											, -		1							
2029 18,7 8 8 1,658 2 1 908 3 2 2,178 2 1 424 1950 42,000 49,119											, -		1							
2030 19.0 8					,						, -		1						,	-, -
2032 19.5 8		19.0	8	8		2	1	908	3		2,178		1	424				1950		49,119
2033 19.8 8 8 1.658 2 1 908 3 2 2.178 2 1 424	2031	19.3	8	8	1,658	2	1	908	3	2	2,178	2	1	424				1950	42,000	49,119
2034 20.0 8	2032	19.5	8	8	1,658	2	1	908	3	2	2,178	2	1	424				1950	42,000	49,119
2035 20.8 8 8 1,658 2 1 908 5 4 4,357 3 2 849 1950 58,300 68,021 2037 20,9 8 8 1,658 2 1 908 5 4 4,357 3 2 849 1950 58,300 68,021 2038 21,1 8 8 1,658 2 1 908 5 4 4,357 3 2 849 1950 58,300 68,021 2033 21,4 8 8 1,658 2 1 908 5 4 4,357 3 2 849 1950 58,300 68,021 2041 22,0 8 8 1,658 2 1 908 5 4 4,357 3 2 849 1950 58,300 68,021 2042 22,3 8 8 1,658 2 1 908				8				908					1							
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2060 28.4 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2061 28.7 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2062 29.1 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2063 29.5 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2064 29.9 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>1</td> <td></td>										1										
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2062 29.1 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2063 29.5 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2064 29.9 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713																				
2063 29.5 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2064 29.9 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713																				
2064 29.9 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713 2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713		_								_										
2065 30.3 8 8 1,658 2 1 908 5 4 4,357 3 2 849 3 2 1,691 1950 70,300 81,713							-			<u> </u>										
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									Option 3 C	perating Cos	st								
	>	Equ	ualization Mi	ixing	Equalia	zation Tank	pumps	(Cloth Media Fi	lter	В	ackwash pum	ps	Efflu	uent pum	ps	HVAC	Repa annu repla cost	To
Year	Average Flow	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Filter Building	Repairs and annual replacement cost	Total Cost
									Option 9 C	perating Cos	st								
	₽	Equ	ualization Mi	ixing	Equalia	zation Tank	pumps		Fourth Clarifi	er	Efflue	nt Filtration pa	ckage	Efflu	uent Pum	ps	HVAC	Repairs annual replace cost	Tota
Year	Average Flow	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Total units	Duty units	Yearly Cost	Filter Building	Repairs and annual replacement cost	Total Cost
2018	15.9	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2019 2020	16.2 16.5	<u>8</u> 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1	995 995				1950 1950	35,800 35,800	43,489 43,489
2020	16.8	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2022	17.1	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2023 2024	17.3 17.5	<u>8</u> 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	1 1	1 1	995 995				1950 1950	35,800 35,800	43,489 43,489
2025	17.8	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2026	18.0	8	8	1,658	2	1	908	1	1	2,178	11	11	995				1950	35,800	43,489
2027 2028	18.3 18.5	<u>8</u> 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	1 1	1 1	995 995				1950 1950	35,800 35,800	43,489 43,489
2029	18.7	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2030	19.0	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2031	19.3	8	8	1,658	2	1	908	1	1	2,178	1	1 1	995				1950	35,800	43,489
2032 2033	19.5 19.8	8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1	995 995				1950 1950	35,800 35,800	43,489 43,489
2034	20.0	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2035	20.3	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2036 2037	20.6 20.9	8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	1 1	1 1	995 995				1950 1950	35,800 35,800	43,489 43,489
2038	21.1	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2039	21.4	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2040 2041	21.7 22.0	<u>8</u> 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1 1	995 995				1950 1950	35,800 35,800	43,489 43,489
2041	22.3	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2043	22.6	8	8	1,658	2	1	908	1	1	2,178	1	1	995				1950	35,800	43,489
2044	22.9	8	8	1,658	2	1	908	1	1	2,178	11	1	995	3	2	1,691	1950	47,800	57,180
2045 2046	23.2 23.5	8 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1 1	995 995	3	2	1,691 1,691	1950 1950	47,800 47,800	57,180 57,180
2047	23.8	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2048	24.2	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2049 2050	24.5 24.8	8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1 1	995 995	3	2	1,691 1,691	1950 1950	47,800 47,800	57,180 57,180
2050	25.1	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2052	25.5	8	8	1,658	2	1	908	1	1	2,178	11	1	995	3	2	1,691	1950	47,800	57,180
2053 2054	25.8 26.2	8	8	1,658 1,658	2	1	908	1	1 1	2,178	1	1 1	995 995	3	2	1,691 1,691	1950 1950	47,800 47,800	57,180 57,180
2054	26.2	8	8	1,658	2	1	908 908	1	1 1	2,178 2,178	<u>1</u> 1	1 1	995	3	2	1,691	1950	47,800	57,180
2056	26.9	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2057	27.2	8	8	1,658	2	1	908	1	1	2,178	11	1 1	995	3	2	1,691	1950	47,800	57,180
2058 2059	27.6 28.0	<u>8</u> 8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	1 1	1 1	995 995	3	2	1,691 1,691	1950 1950	47,800 47,800	57,180 57,180
2060	28.4	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2061	28.7	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2062	29.1 29.5	8	8	1,658	2	1	908	1	1	2,178	<u>1</u>	1	995	3	2	1,691 1,691	1950 1950	47,800 47,800	57,180 57,180
2063 2064	29.5	8	8	1,658 1,658	2	1	908 908	1	1 1	2,178 2,178	1	1 1	995 995	3	2	1,691	1950	47,800	57,180
2065	30.3	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180
2066	30.7	8	8	1,658	2	1	908	1	1	2,178	1	1	995	3	2	1,691	1950	47,800	57,180 50,000

Net Present Value Calculation

NPV Basis

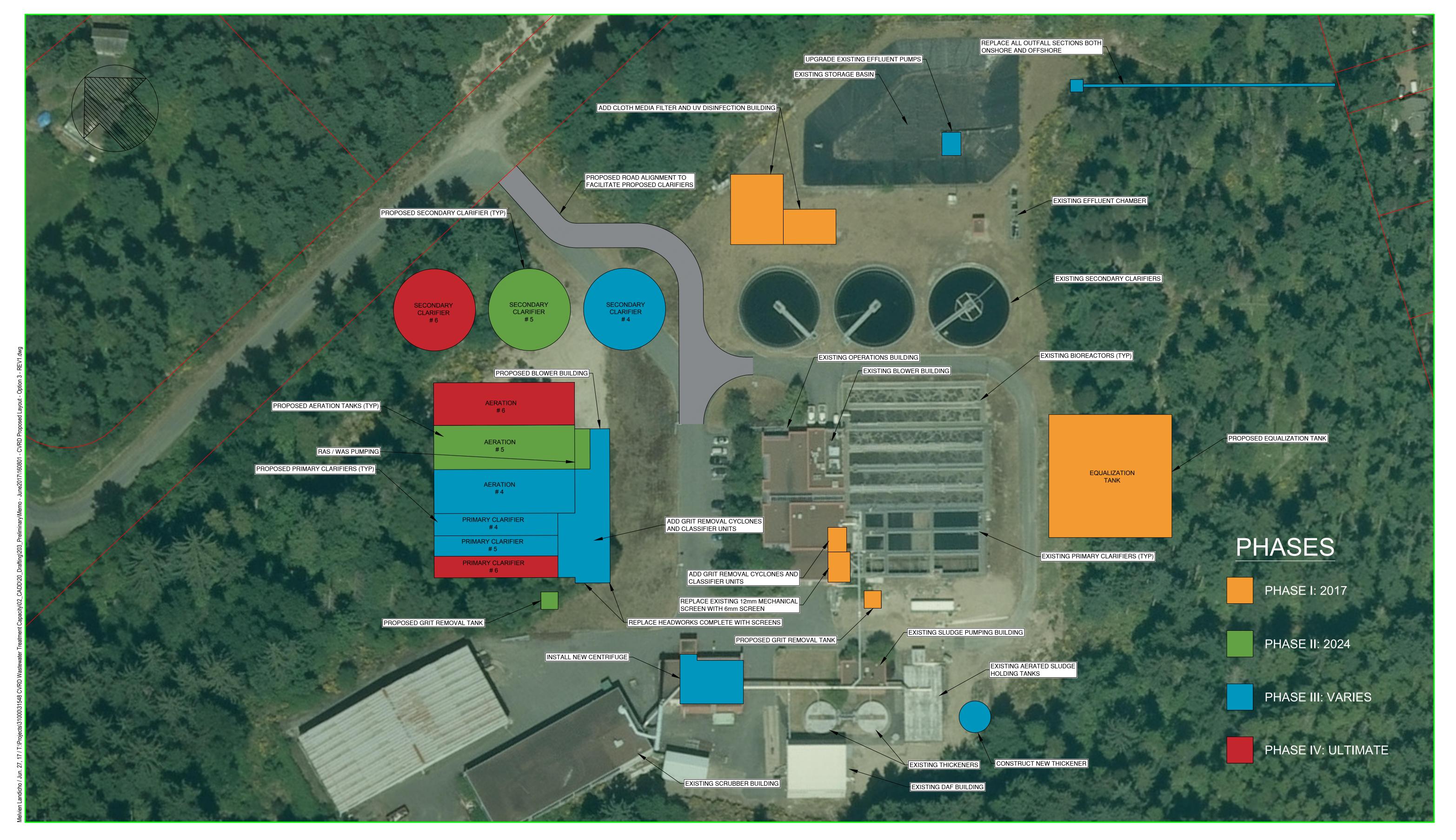
Discount rate =

0.04

Inflation = 2%

				Opti	on 3									
	Project Year	Ca	pital Cost	O&M Cost		Total Cost	Inflated Cost		Capital Cost	Option O&M Cost	Total Cost		Inflated Cost	Inflation Factor 2%
2017	1	\$	15,489,000		\$		\$	\$	12,327,000		\$ 12,327,000) '	\$ 12,573,540	1.02
2017	2	Ψ	13,409,000	\$ 49,119			\$ 	Ψ	12,327,000	\$ 43,489	\$ 43,489	_	\$ 45,246	1.04
2019	3			\$ 49,119		49,119	\$			\$ 43,489	\$ 43,489	_	\$ 46,151	1.06
2020	4			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 47,074	1.08
2021	5			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 48,015	1.10
2022	6			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 48,976	1.13
2023	7			\$ 49,119		49,119	\$			\$ 43,489	\$ 43,489	_	\$ 49,955	1.15
2024	8	\$	6,610,000	\$ 49,119			\$	\$	6,610,000	\$ 43,489	\$ 6,653,489	_	\$ 7,795,623	1.17
2025	9	Ψ	0,010,000	\$ 49,119			\$	Ψ	0,010,000	\$ 43,489	\$ 43,489	_	\$ 51,973	1.20
2026	10			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 53,013	1.22
2027	11			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 54,073	1.24
2028	12			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 55,155	1.27
2029	13			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 56,258	1.29
2030	14			\$ 49,119			\$			\$ 43,489	\$ 43,489	_	\$ 57,383	1.32
2031	15	\$	19,529,000	\$ 49,119		19,578,119	\$	\$	19,529,000	\$ 43,489	\$ 19,572,489	_	\$ 26,341,993	1.35
2032	16	Ψ	10,020,000	\$ 49,119	\$	49,119	\$	Ψ	10,020,000	\$ 43,489	\$ 43,489		\$ 59,701	1.37
2033	17	\$	10,712,000	\$ 49,119		10,761,119	\$	\$	10,712,000	\$ 43,489	\$ 10,755,489		\$ 15,060,281	1.40
2034	18	\$	2,463,000	\$ 49,119		2,512,119	\$	\$	-	\$ 43,489	\$ 43,489	_	\$ 62,113	1.43
2035	19			\$ 68,021	\$	68,021	\$			\$ 43,489	\$ 43,489	_	\$ 63,355	1.46
2036	20			\$ 68,021	\$	68,021	\$			\$ 43,489	\$ 43,489	_	\$ 64,623	1.49
2037	21			\$ 68,021		68,021	\$			\$ 43,489	\$ 43,489	_	\$ 65,915	1.52
2038	22			\$ 68,021		68,021	\$			\$ 43,489	\$ 43,489	_	\$ 67,233	1.55
2039	23			\$ 68,021		68,021	\$			\$ 43,489	\$ 43,489	_	\$ 68,578	1.58
2040	24			\$ 68,021	\$	68,021	\$			\$ 43,489	\$ 43,489	_	\$ 69,949	1.61
2041	25			\$ 68,021	\$	68,021	\$			\$ 43,489	\$ 43,489	_	\$ 71,348	1.64
2042	26			\$ 68,021	\$	68,021	\$			\$ 43,489	\$ 43,489	_	\$ 72,775	1.67
2043	27	\$	2,492,000	\$ 68,021	\$	2,560,021	\$ 4,369,666	\$	2,492,000	\$ 43,489	\$ 2,535,489	9 :	\$ 4,327,792	1.71
2044	28			\$ 81,713	\$	81,713	\$ 142,264			\$ 57,180	\$ 57,180) ;	\$ 99,552	1.74
2045	29	\$	2,667,000	\$ 81,713	\$	2,748,713	\$ 4,881,287	\$	2,667,000	\$ 57,180	\$ 2,724,180) :	\$ 4,837,721	1.78
2046	30			\$ 81,713	\$	81,713	\$ 148,011			\$ 57,180	\$ 57,180) :	\$ 103,574	1.81
2047	31			\$ 81,713	\$	81,713	\$ 150,971			\$ 57,180	\$ 57,180) :	\$ 105,645	1.85
2048	32			\$ 81,713	\$	81,713	\$ 153,991			\$ 57,180	\$ 57,180) :	\$ 107,758	1.88
2049	33			\$ 81,713	\$	81,713	\$ 157,070			\$ 57,180	\$ 57,180) :	\$ 109,913	1.92
2050	34			\$ 81,713	\$	81,713	\$ 160,212			\$ 57,180	\$ 57,180) :	\$ 112,112	1.96
2051	35			\$ 81,713	\$	81,713	\$ 163,416			\$ 57,180	\$ 57,180) :	\$ 114,354	2.00
2052	36			\$ 81,713	\$	81,713	\$ 166,684			\$ 57,180	\$ 57,180) :	\$ 116,641	2.04
2053	37			\$ 81,713	\$	81,713	\$ 170,018			\$ 57,180	\$ 57,180) :	\$ 118,974	2.08
2054	38			\$ 81,713	\$	81,713				\$ 57,180	\$ 57,180) :	\$ 121,353	2.12
2055	39			\$ 81,713	\$	81,713	\$ 176,887			\$ 57,180	\$ 57,180) :	\$ 123,780	2.16
2056	40	\$	1,501,000	\$ 81,713	\$	1,582,713	\$ 3,494,692	\$	1,501,000	\$ 57,180	\$ 1,558,180)	\$ 3,440,524	2.21
2057	41			\$ 81,713	\$	81,713	\$ 184,033			\$ 57,180	\$ 57,180)	\$ 128,781	2.25
2058	42			\$ 81,713	\$	81,713				\$ 57,180	\$ 57,180)	\$ 131,357	2.30
2059	43			\$ 81,713	\$	81,713	\$ 191,468			\$ 57,180	\$ 57,180) [\$ 133,984	2.34
2060	44	\$	1,666,000	\$ 81,713		1,747,713		\$	1,666,000	\$ 57,180	\$ 1,723,180)	\$ 4,118,492	2.39
2061	45			\$ 81,713	\$	81,713				\$ 57,180	\$ 57,180) [\$ 139,397	2.44
2062	46			\$ 81,713	\$	81,713	\$ 203,187			\$ 57,180	\$ 57,180) [\$ 142,185	2.49
2063	47	\$	5,955,000	\$ 81,713	\$	6,036,713	\$ 15,311,177	\$	5,955,000	\$ 57,180	\$ 6,012,180) [\$ 15,248,954	2.54
2064	48			\$ 81,713	\$	81,713	\$ 211,396			\$ 57,180	\$ 57,180) :	\$ 147,929	2.59
2065	49			\$ 81,713	\$	81,713	\$ 215,624			\$ 57,180	\$ 57,180) :	\$ 150,888	2.64
2066	50			\$ 81,713	\$	81,713	\$ 219,937			\$ 57,180	\$ 57,180) :	\$ 153,905	2.69
		\$	69,084,000	\$ 67,890		NPV	\$ 53,636,504	\$	63,459,000	\$ 49,916	NPV		\$ 48,311,441	

Appendix B
Drawings



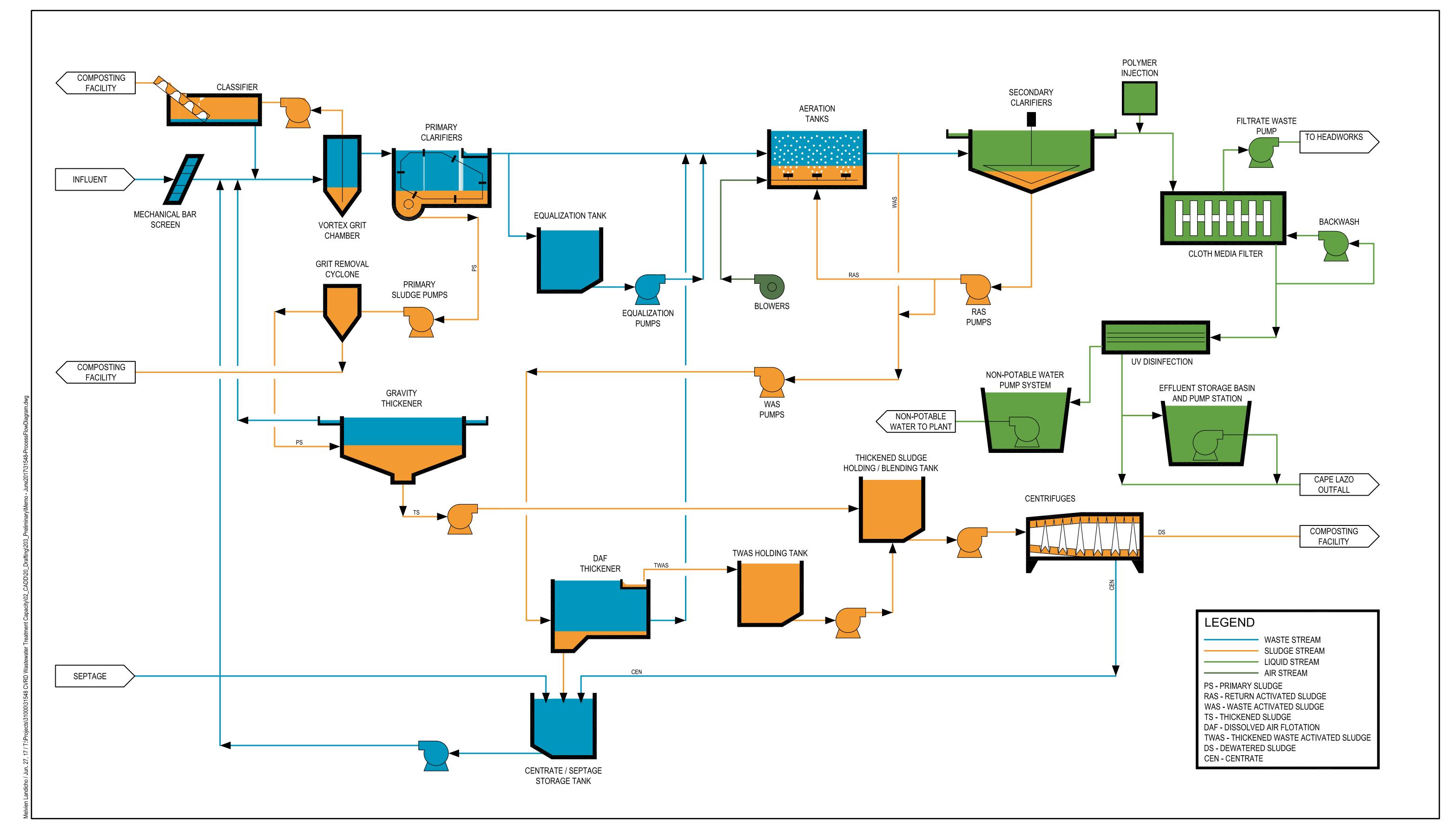


COMOX VALLEY WATER POLLUTION CONTROL CENTER PROPOSED PLANT LAYOUT (OPTION 3)

Figure B.1

PROJECT : 31548

AUGUST 2016



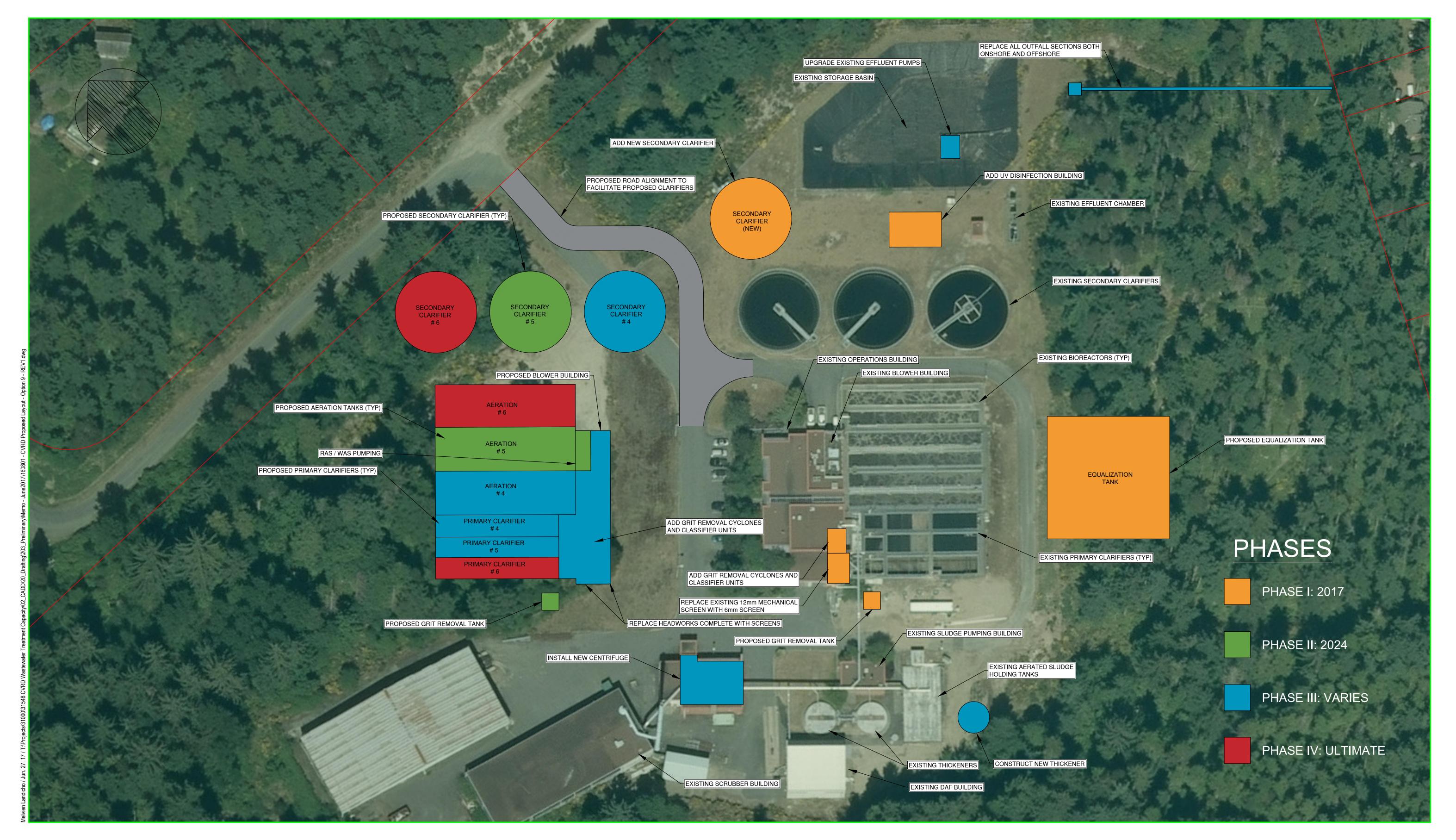


COMOX VALLEY WATER POLLUTION CONTROL CENTER PROCESS FLOW DIAGRAM (OPTION 3)

Figure B.2

PROJECT: 31548

AUGUST 2016



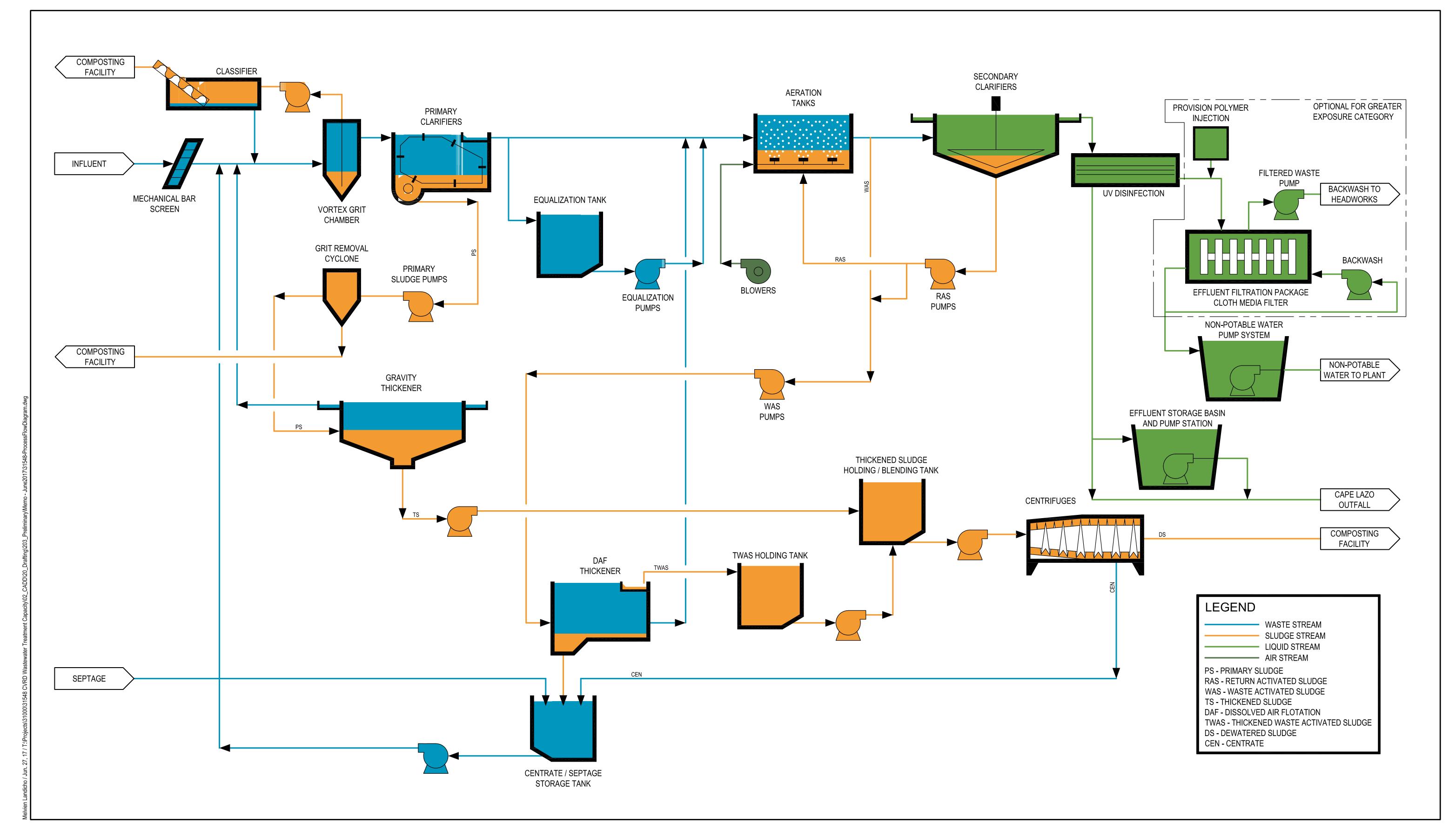


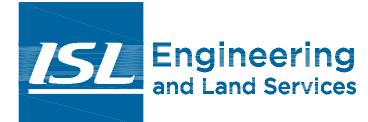
COMOX VALLEY WATER POLLUTION CONTROL CENTER PROPOSED PLANT LAYOUT (OPTION 9)

Figure B.3

PROJECT : 31548

JUNE 2017





COMOX VALLEY WATER POLLUTION CONTROL CENTER PROCESS FLOW DIAGRAM (OPTION 9)

Figure B.4

PROJECT: 31548

AUGUST 2016